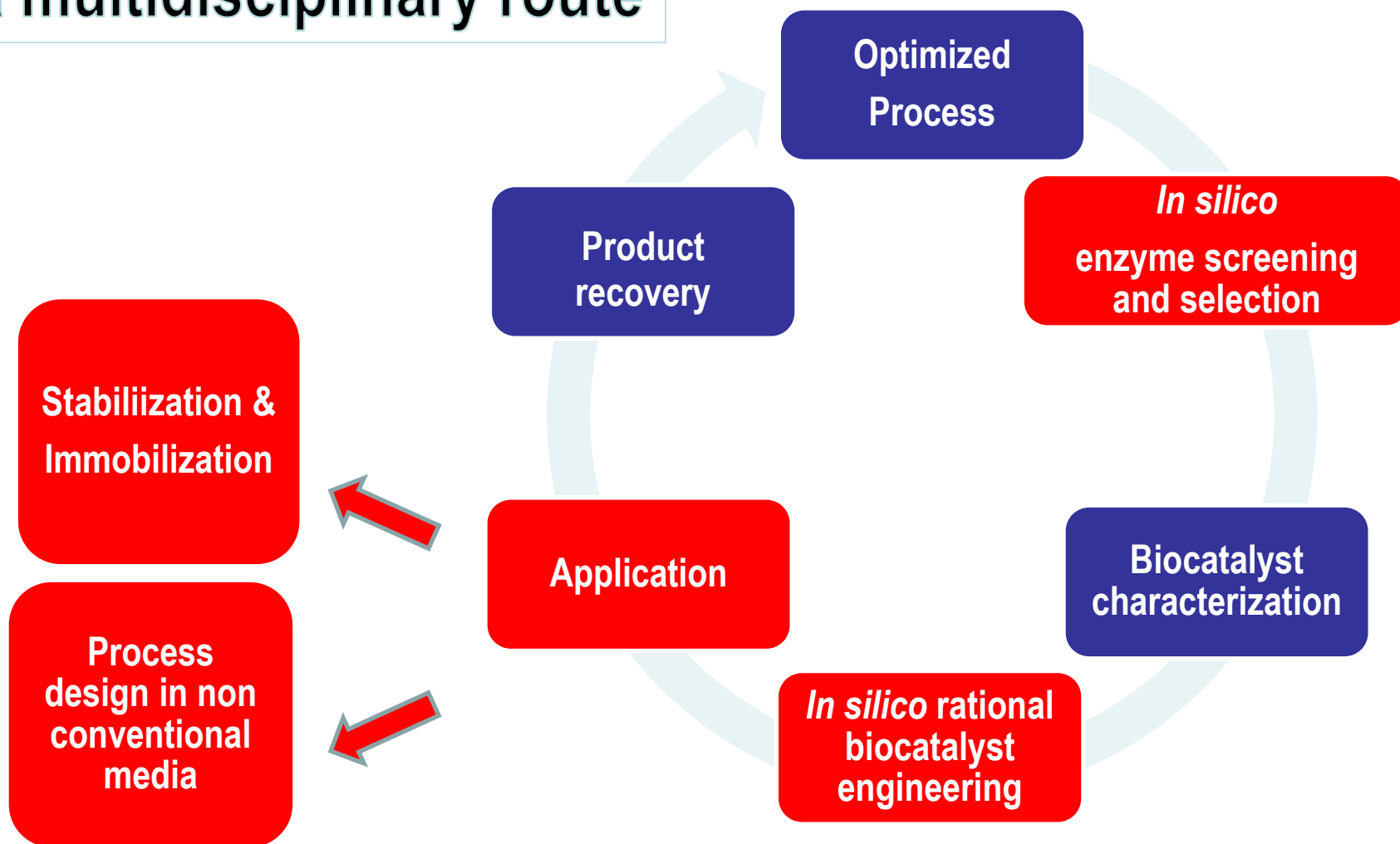


**Biocatalysts in chemical reactions and organic synthesis**

**Strategies for planning rationally biocatalyzed reactions**

# Developing a biocatalyzed process: a multidisciplinary route

## Contribution from chemists?



**The reaction:** identifying the most suitable enzyme and the reaction conditions to carry out the biotransformation at lab-scale (proof of concept)

**The protein:** Trying to predict enzyme properties (stability, activity, selectivity) on a rational basis in order to preserve such features as long as possible throughout the biotransformation

**The process:** how making the enzyme and the biotransformation effective at large (industrial) scale, the process economically viable and environmentally sustainable

**Aim:**  
**making enzymes working under unconventional «desperate» conditions**  
**while keeping most of their catalytic activity**



***Solid to solid:***



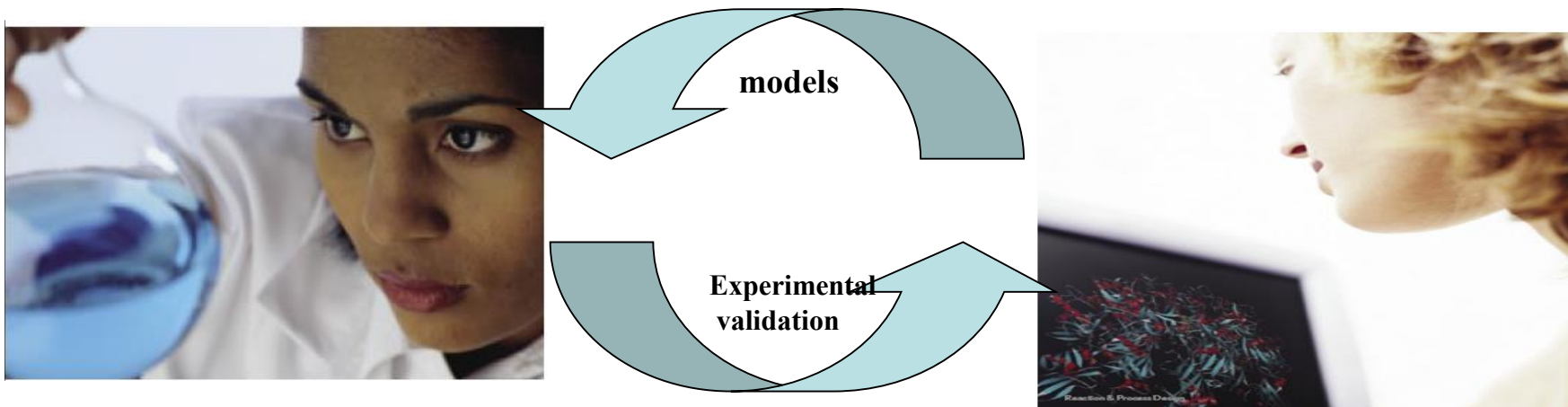
***Organic solvent***



***Bulk –solventless - transformation***



# Integrating experimental and computational methods



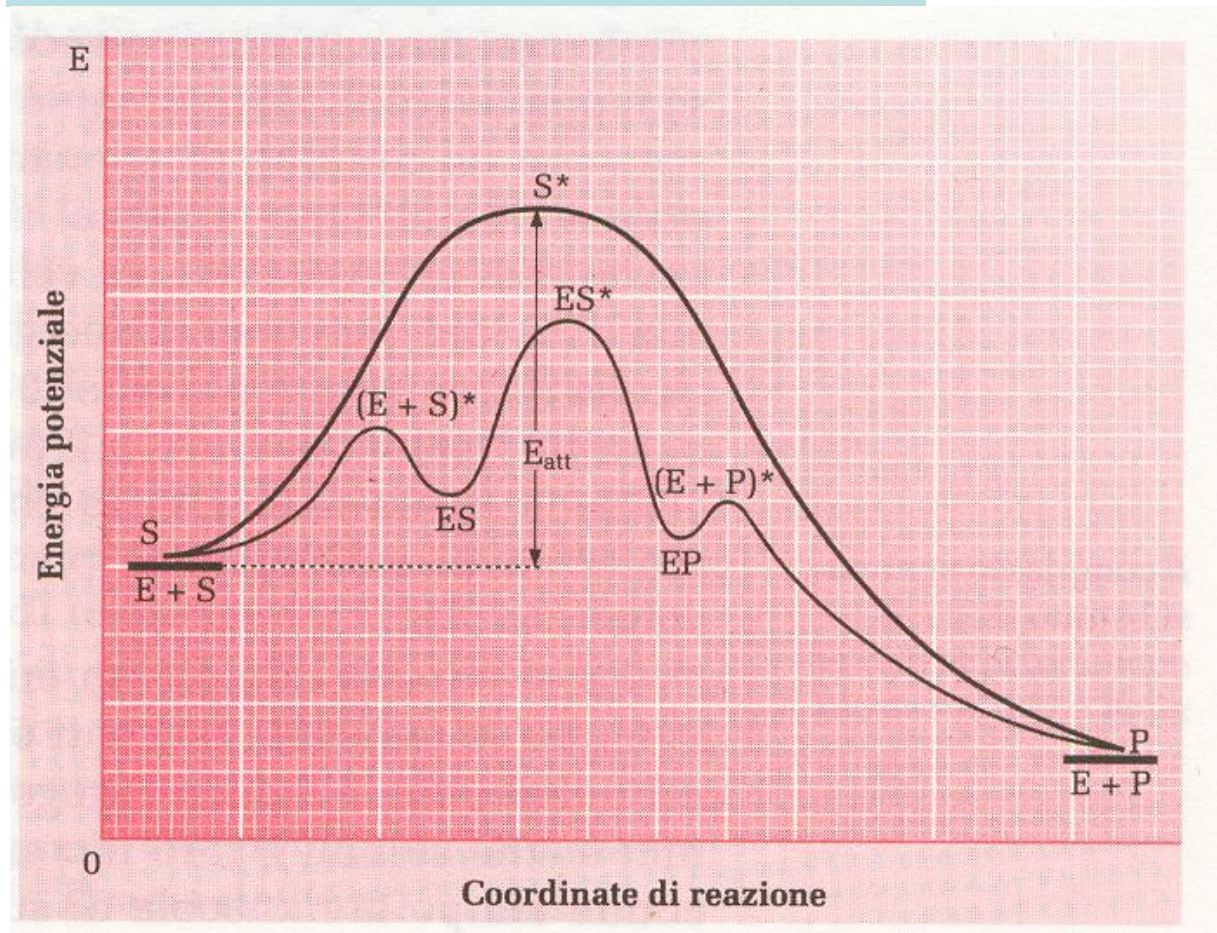
**Computational simulations and predictions must be competitive with experimental approaches & time scale**

**Identifying a suitable enzyme  
and predict its ability to  
transform a certain substrate  
with the desired  
chemo-regio-stereo-selectivity  
(when required)**

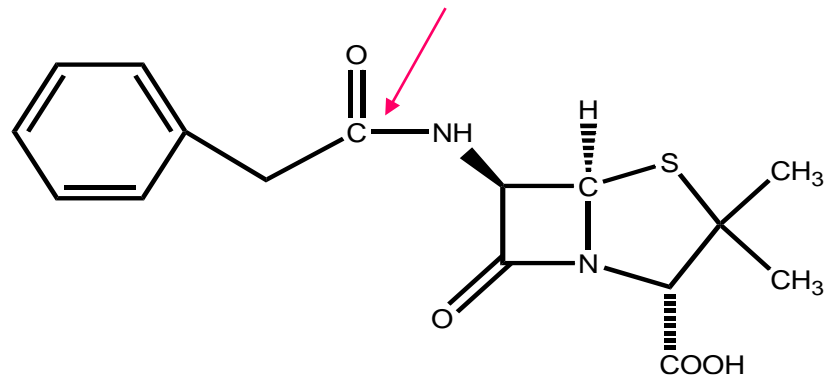
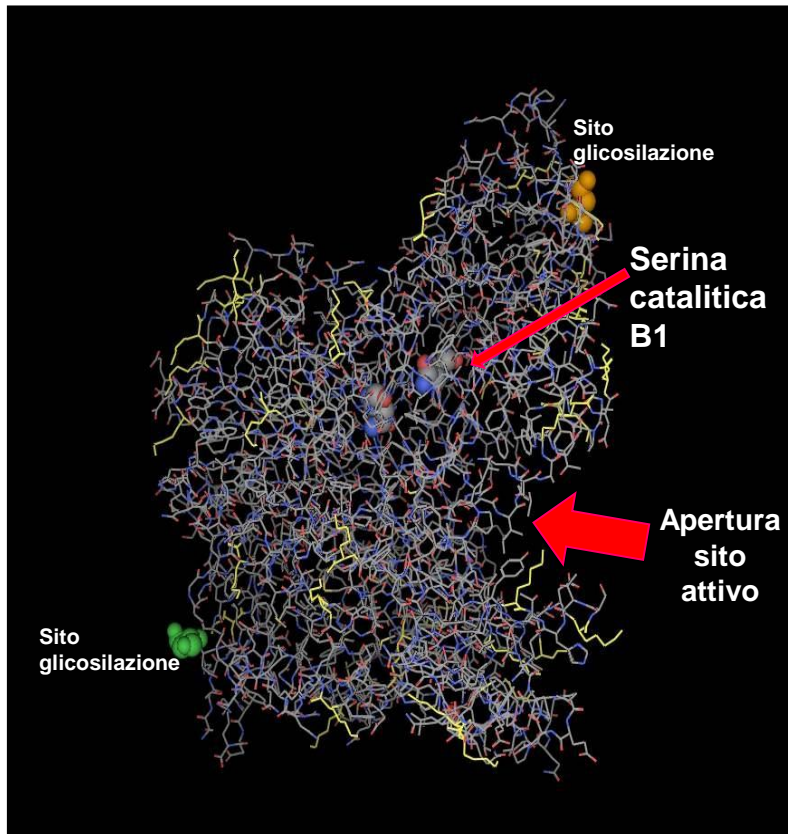
*How can we study and  
predict enzyme properties?*

## The theory:

- 1) Enzyme-substrate recognition
- 2) Catalysis and Transformation



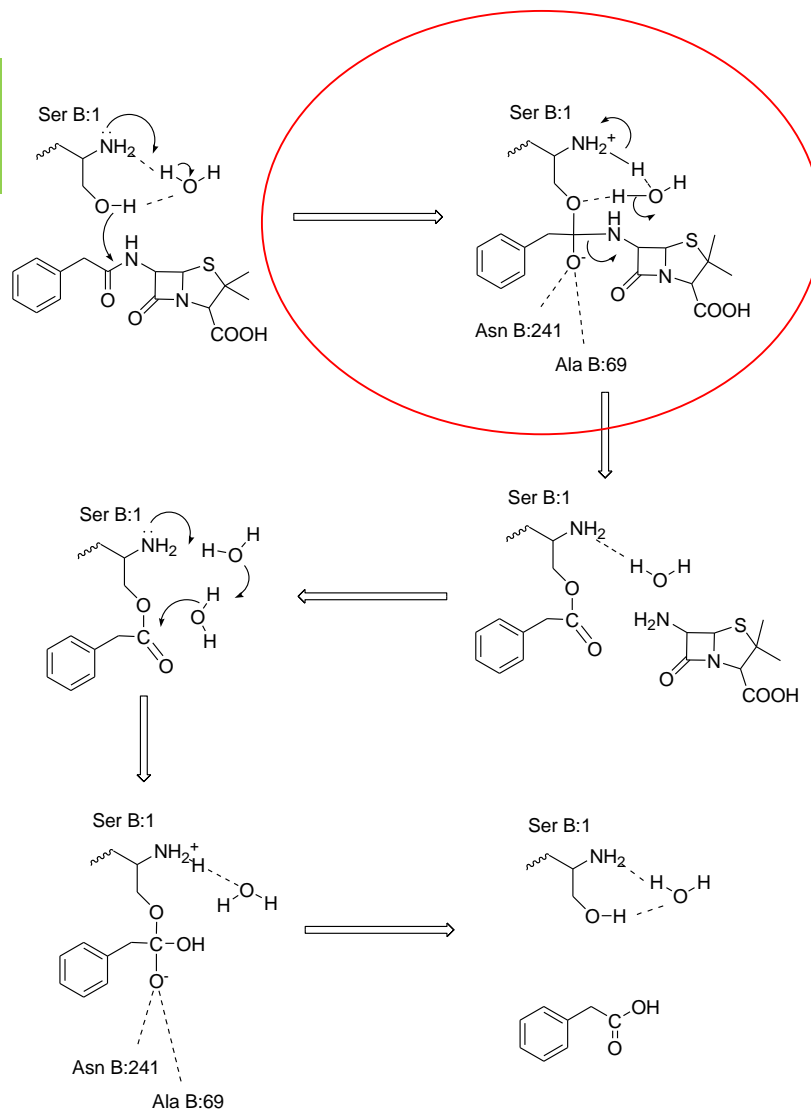
# Molecular simulation for the study of enzyme-substrate recognition: penicillin G inside penicillin G amidase (PGA), a serine hydrolase (dimer)



Penicillin G

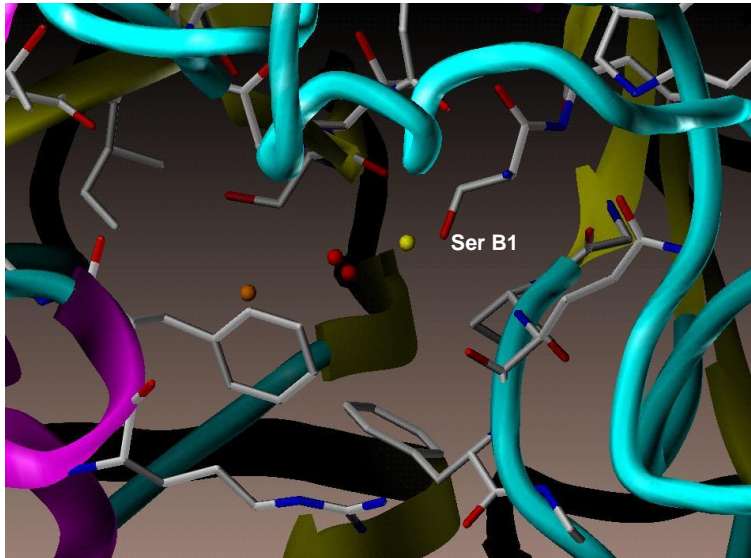


# Mechanism of action of PGA



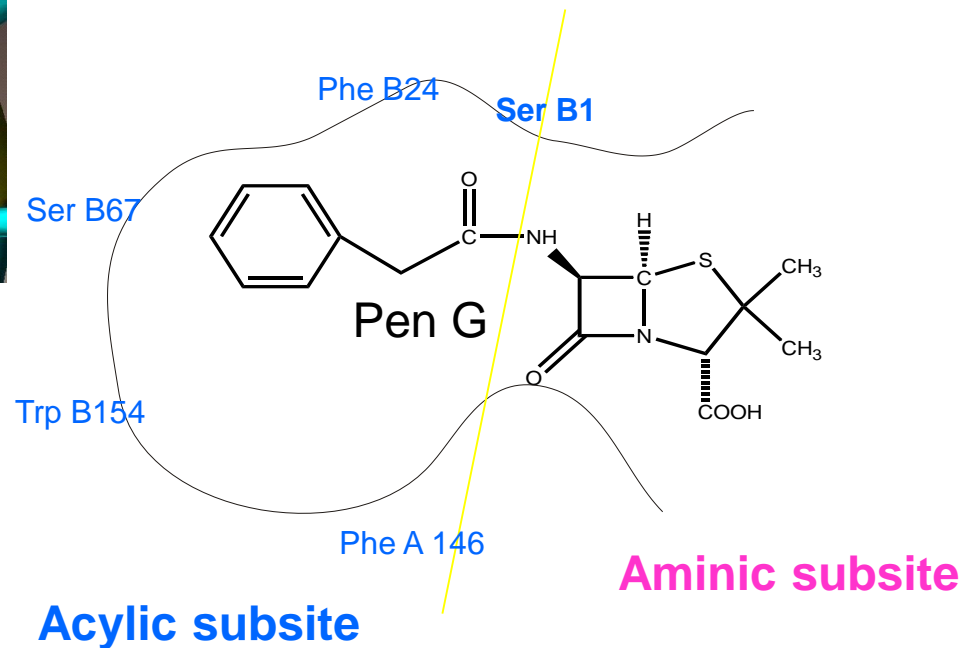
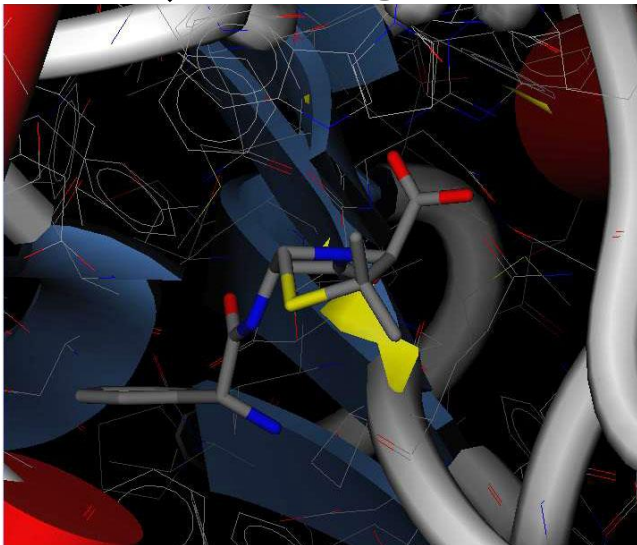
**Tetrahedral intermediate**

# Penicillin G Amidase (PGA) recognizes substrates that are derivatives of phenylacetic acid



active site 3D structure with water molecules

↓ Docking the substrate



Docking simulates enzyme-  
substrate recognition:  
affinity,  $K_m$

# What is not accounted by docking?

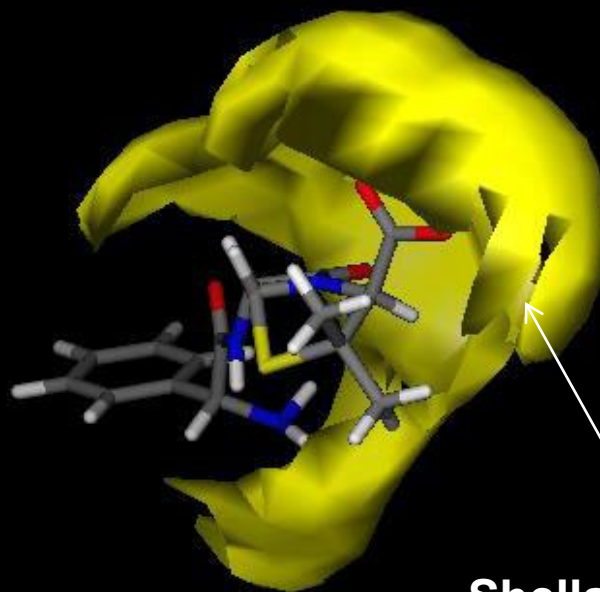
**Physical chemical factors mostly related to solvation, desolvation, partition, diffusion**

- In the active site of the enzyme***
- On the surface of the enzymes***

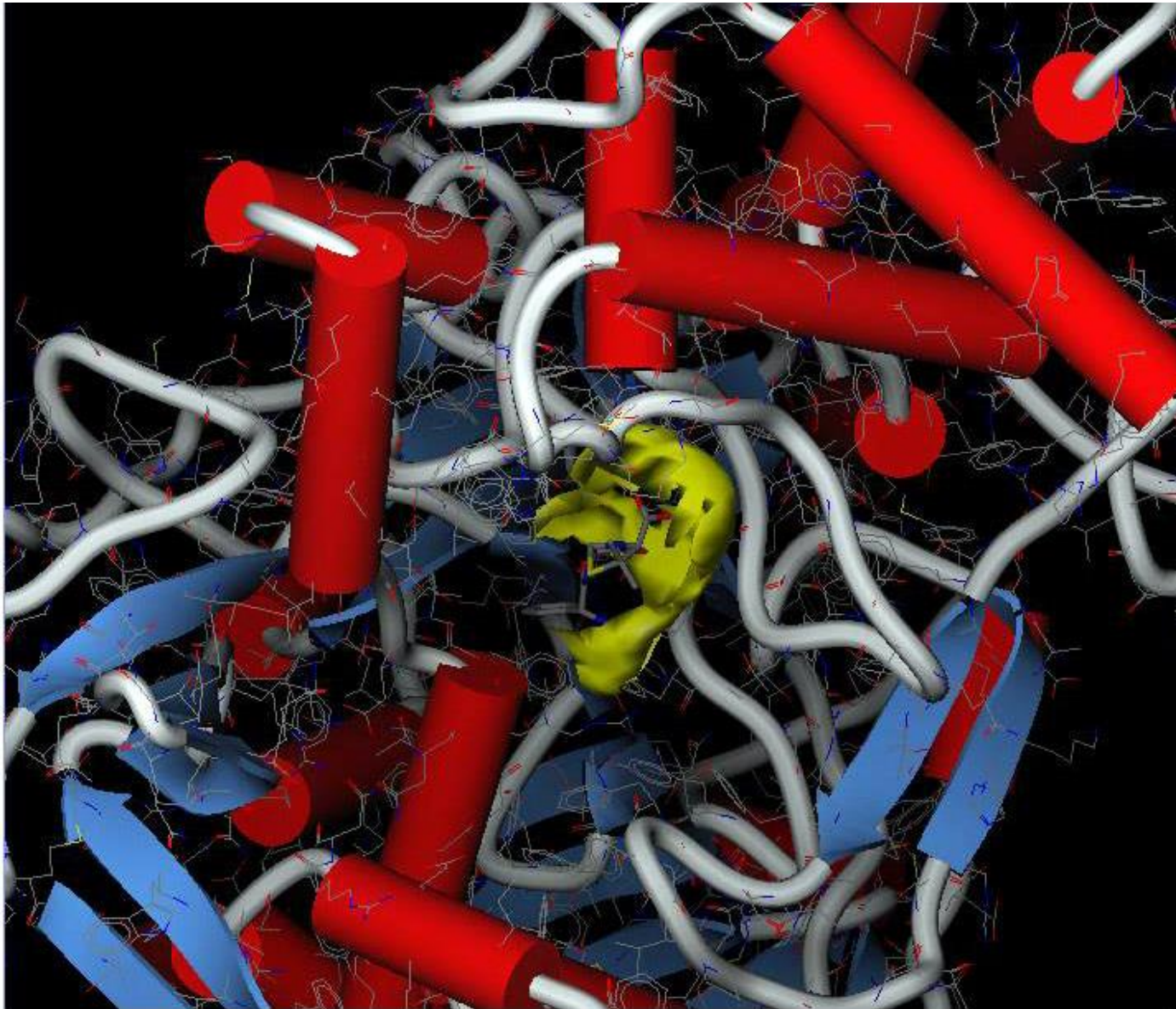
**This is particularly relevant when enzymes work as heterogeneous catalysts, suspended in the medium**

1.

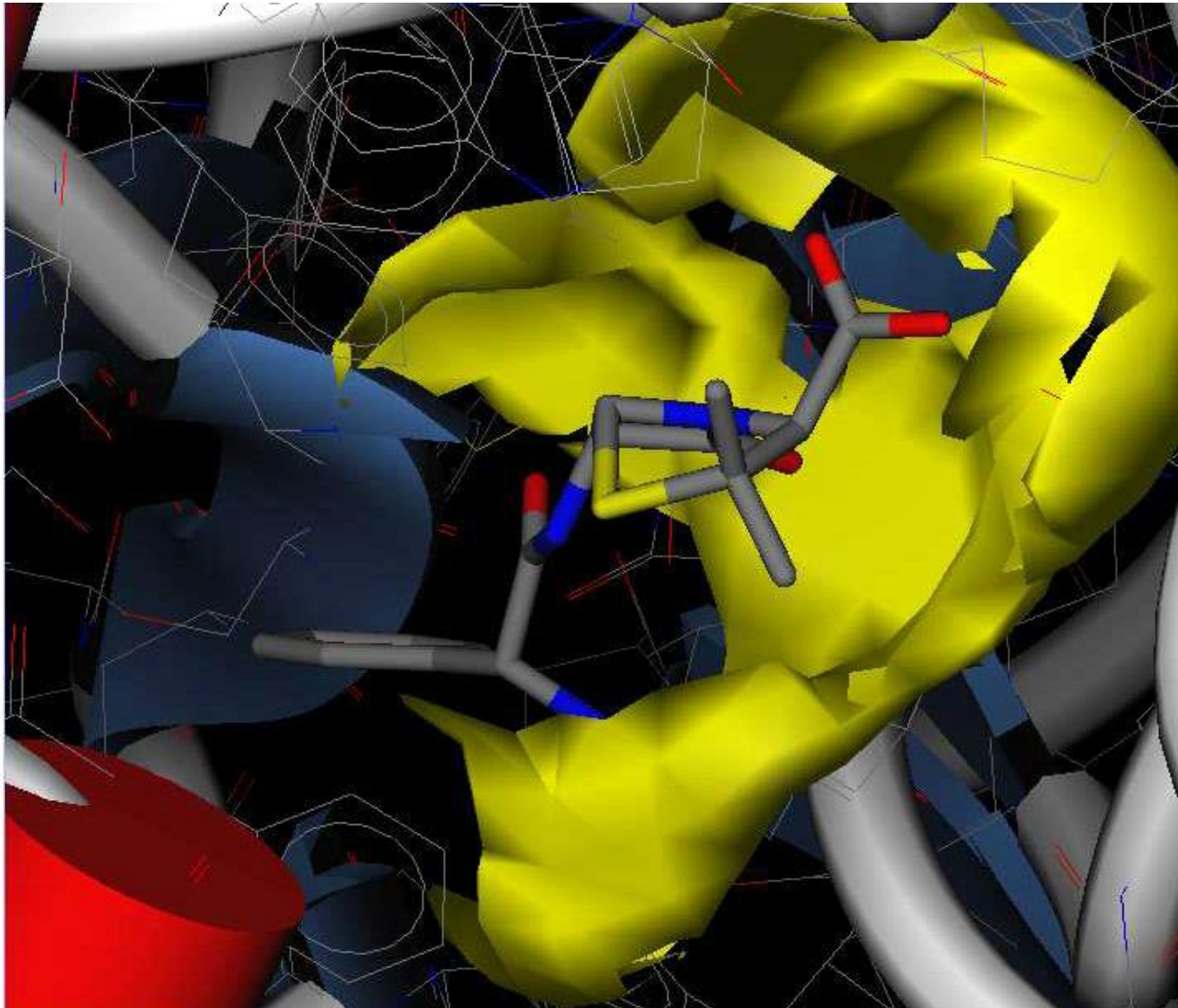
## Penicillin before enzyme-substrate recognition



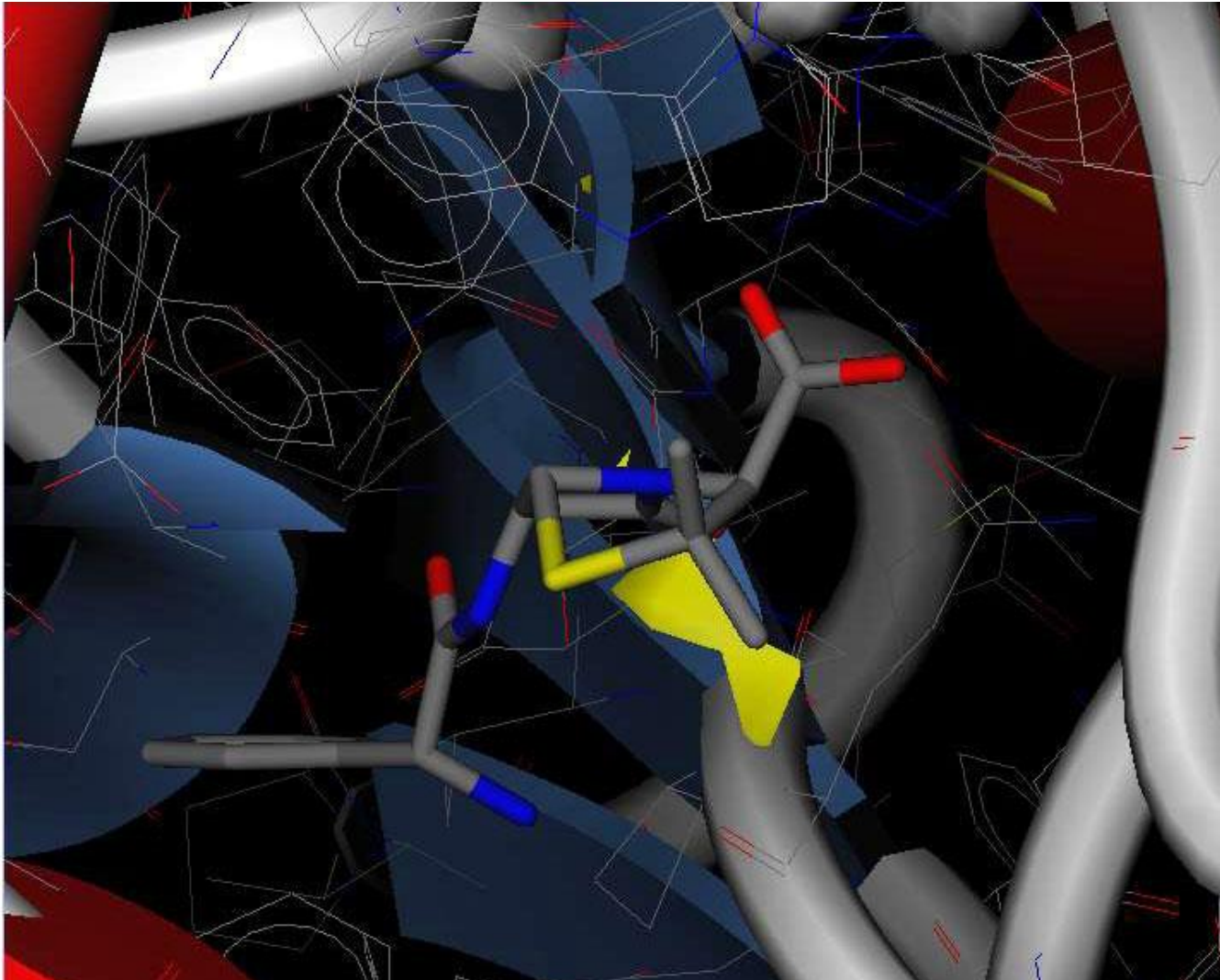
Shells of water  
solvating the substrate  
in the aqueous bulk  
medium



**2. The substrate enters the active site**

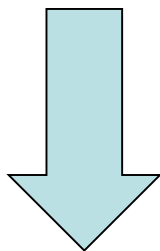


**3. To enable enzyme substrate interactions/recognition, part of the water molecules must be displaced (desolvation)**



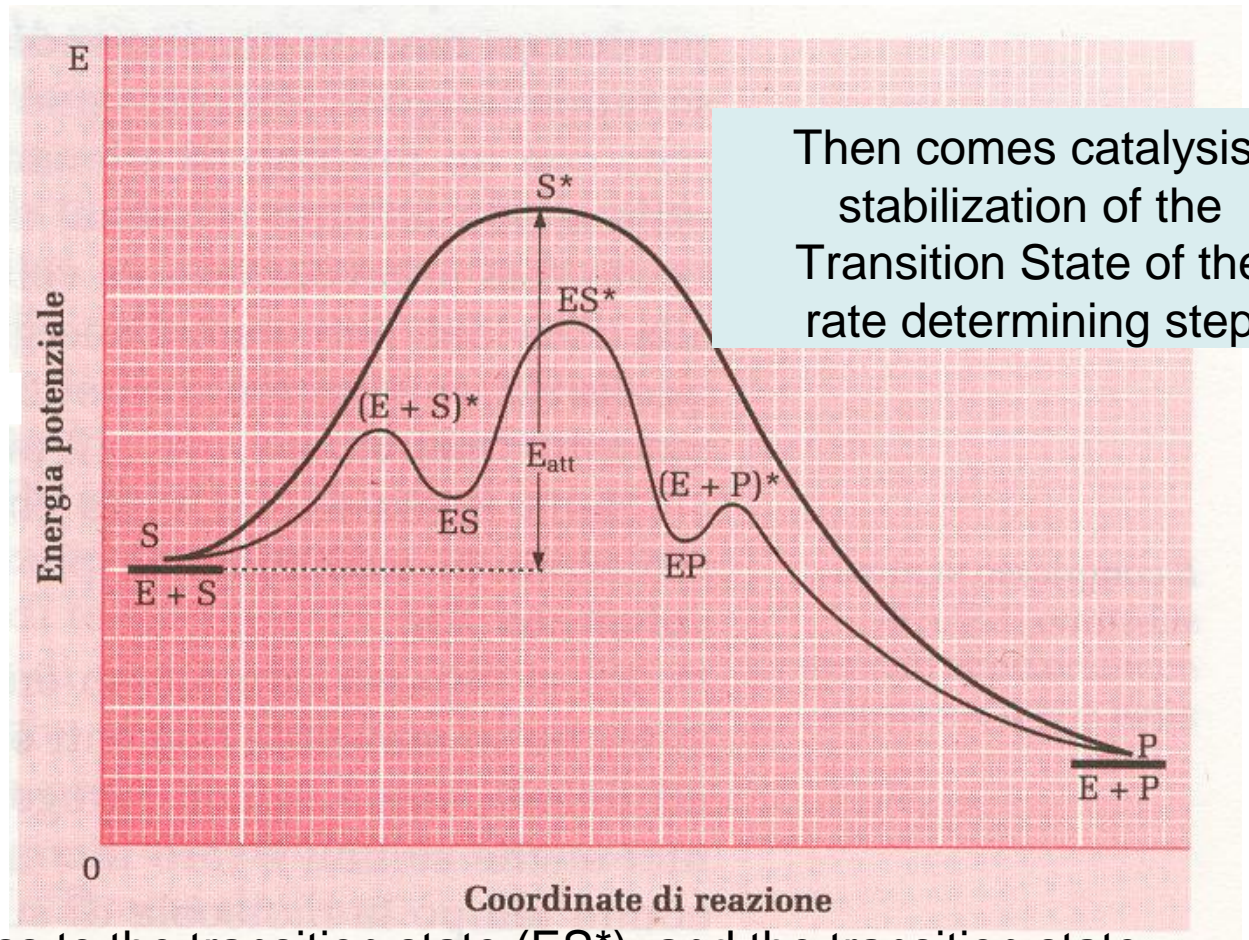
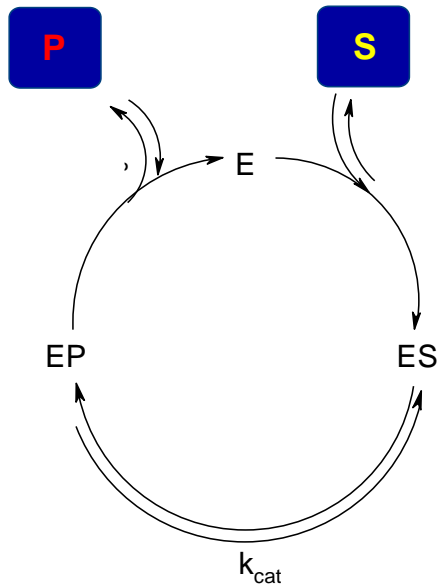
**4. After displacement of water molecules, the substrate establish new electrostatic interactions with residues in the active site**

Then comes catalysis: stabilization of the Transition State of the rate determining step



**Kinetics !!!!**



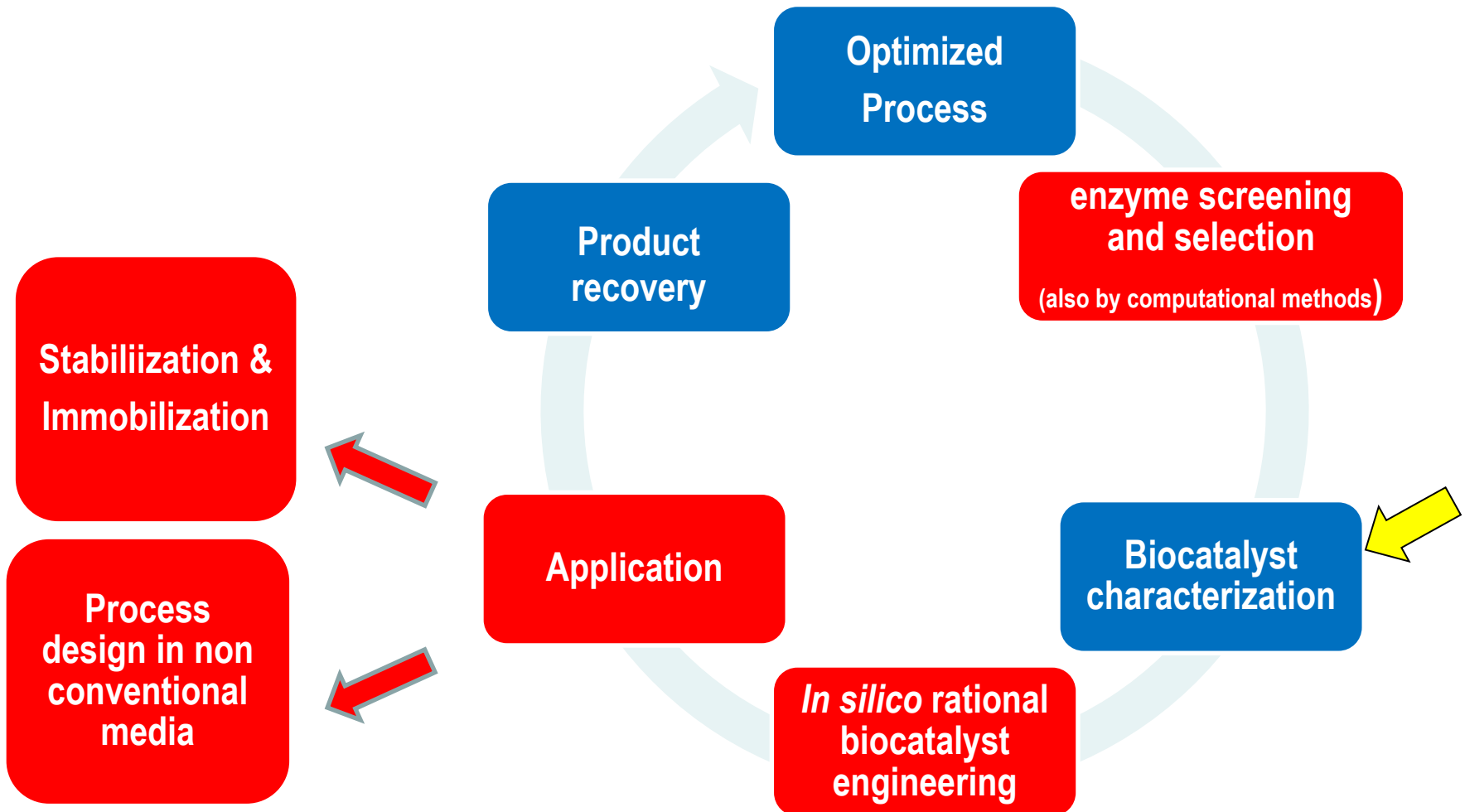


Then comes catalysis:  
stabilization of the  
Transition State of the  
rate determining step

ES complex must pass to the transition state ( $ES^*$ ); and the transition state complex must advance to an enzyme product complex (EP). The latter is finally competent to dissociate to product and free enzyme. The series of events can be shown as:



Enzymes are characterized by enzymologists in diluted buffers, therefore in conditions quite distant from the operational conditions in industry



Most often biocatalysts are used under non physiological conditions, the so called:

# non conventional media

*.....anything different from a dilute aqueous solution.*

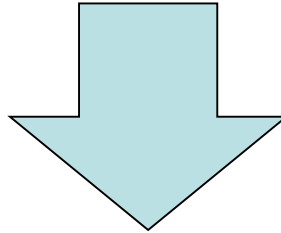
*Most often a **multi-phase system**, some examples:*

Neat  
substrates  
+  
Native  
enzyme  
+  
Traces of  
solvent



Neat  
substrates  
+  
Immobilized  
enzyme

**The point of view of kinetic studies  
in fundamental enzymology:  
enzyme solubilized in buffer**



**Most often models developed by enzymologists  
cannot be used in applied biocatalysis**

**Mass transfer and diffusion limitations are most often rate determining**

# Parameters and equation refer to simplified ideal conditions

## Equazione di Michaelis – Menten (1913)



Leonor Michaelis  
(1875–1949)

$$V = k_{\text{cat}} [E]_{\text{T}} \frac{[S]}{K_S + [S]}$$

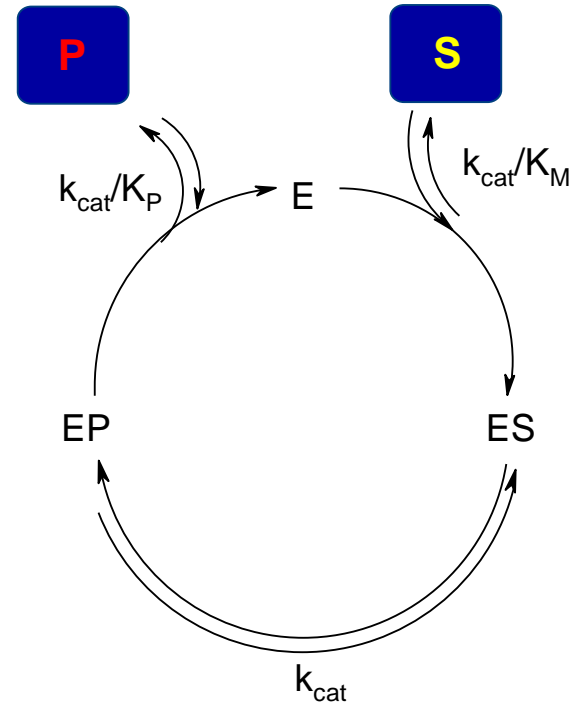
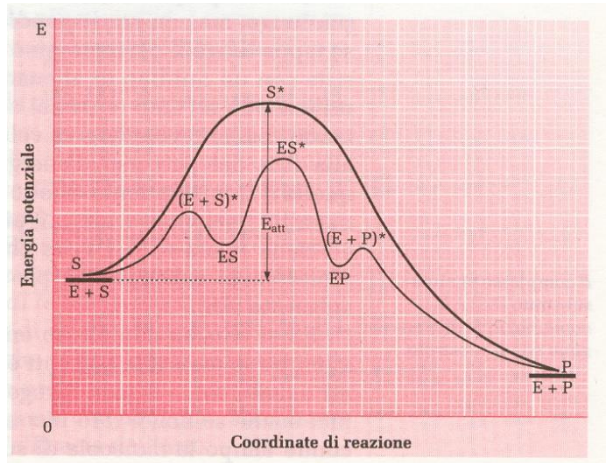


Maud Leonora Menten  
(1879–1960)

oppure

$$v = V_{\text{max}} \frac{[S]}{K_M + [S]}$$

**Parameters that  
describe enzyme  
efficiency in  
biocatalysis**



**Specific activity:  $k_{cat}$**

$k_{cat}$  (time<sup>-1</sup>)

**First order rate constant for the conversion of  $ES, ES^*, EP$**

**All species involving  $E$**



**What is really relevant in biocatalysis?  
Turnover number: biocatalyst productivity**

In catalysis it refers to:

**the number of moles of product formed  
per mole of catalyst over the reaction period.**

dimensionless ratio:  
**(mol product) / (mol enzyme)**



# Specificity

$k_{cat}/k_m$  specificity constant

Specific activity

affinity

$K_{cat}/K_M$  must be calculated at low concentration of Substrate, when the enzyme is not saturated

Penicillin G amidase from different microorganisms display different specificity towards pen G

Enzima	Substrato	T(°C)	pH	$k_{cat}/K_M$ (M <sup>-1</sup> s <sup>-1</sup> )
Penicillina amidasi				
<i>E. coli</i>	Penicillina G	25.0	7.8	4 800 000
<i>A. faecalis</i>	Penicillina G	25.0	7.8	10 000 000
<i>K. citrofila</i>	Penicillina G	25.0	7.8	3 000 000

# Selectivity

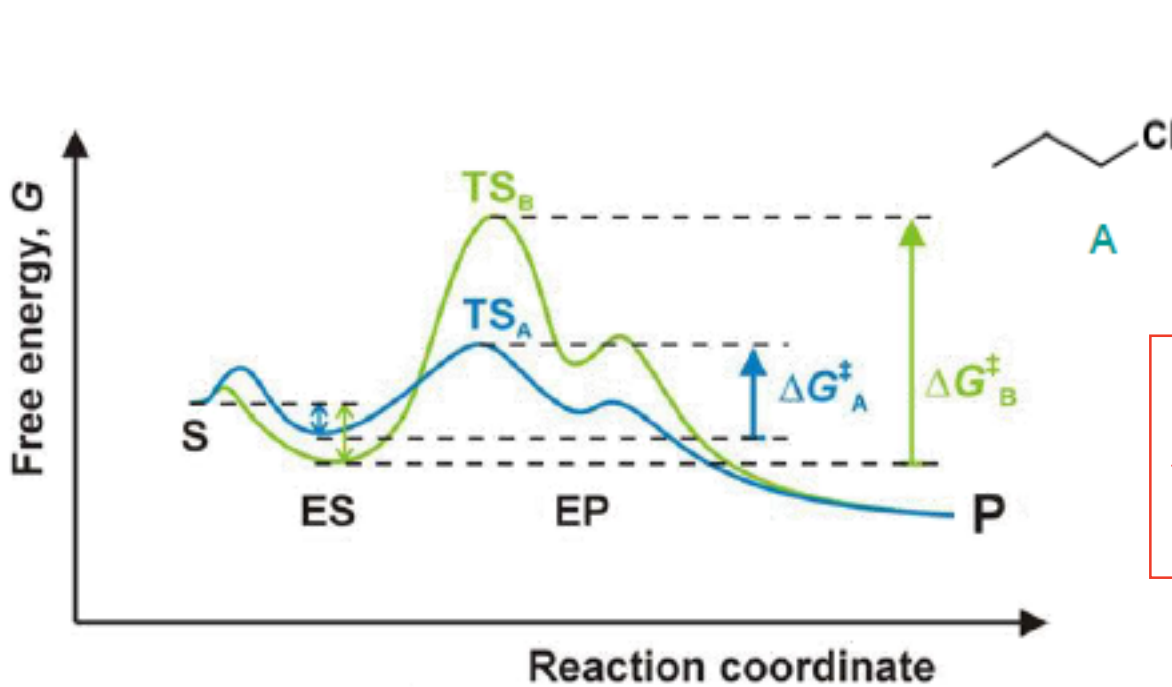
$k_{\text{cat}}/k_{\text{m}}$  specificity  
constant

$$\text{selectivity} = \frac{(k_{\text{cat}}/k_{\text{m}})_A}{(k_{\text{cat}}/k_{\text{m}})_B}$$

Ratio between the  
specificity constants

How the enzyme is able to  
discriminate between A and B  
  
(chemo-regio-enantio-  
selectivity)

# Enzyme selectivity: substrate A vs B



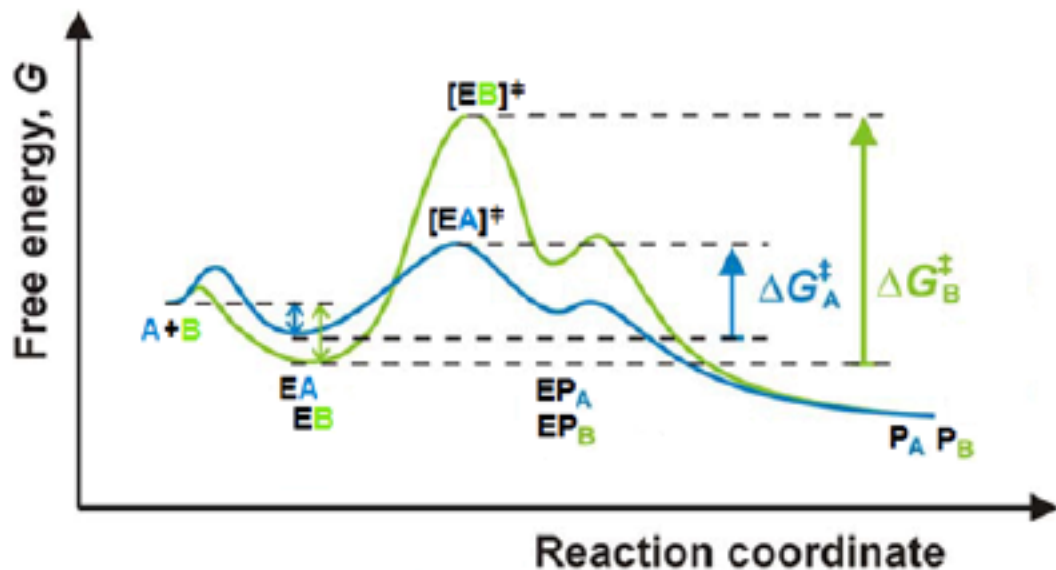
**selettività:**  $\frac{(k_{\text{cat}}/k_m)_A}{(k_{\text{cat}}/k_m)_B}$

Selectivity depends on the  $\Delta\Delta G^\ddagger$  activation of the RATE DETERMINING STEP!

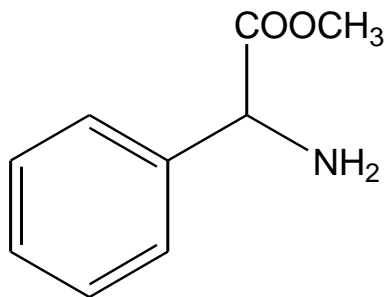
$\Delta\Delta G^\ddagger$  di  $5,71 \text{ kJmol}^{-1} \nu \times 10$

$\Delta\Delta G^\ddagger$  di  $34 \text{ kJmol}^{-1} \nu \times 10^6$

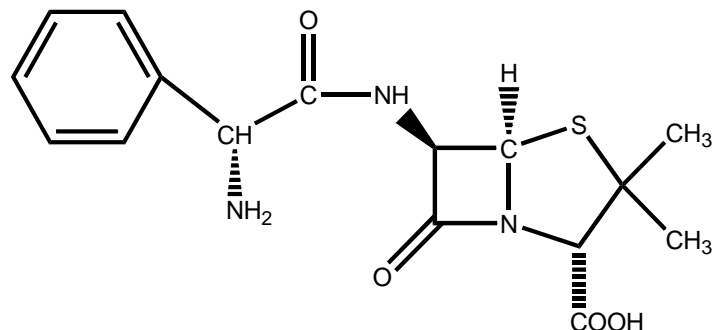
# Enzyme enantioselectivity: enantiomer S vs R



$\Delta\Delta G^\ddagger$ [kcal/mol]	$v_A/v_B$	e.e. [%]
0.118	1.2	10
0.651	3	50
1.74	19	90
2.17	39	95
3.14	199	99
4.50	1,999	99.9



Phenylglycine



Only the R-enantiomer used for ampicillin semi-synthesis

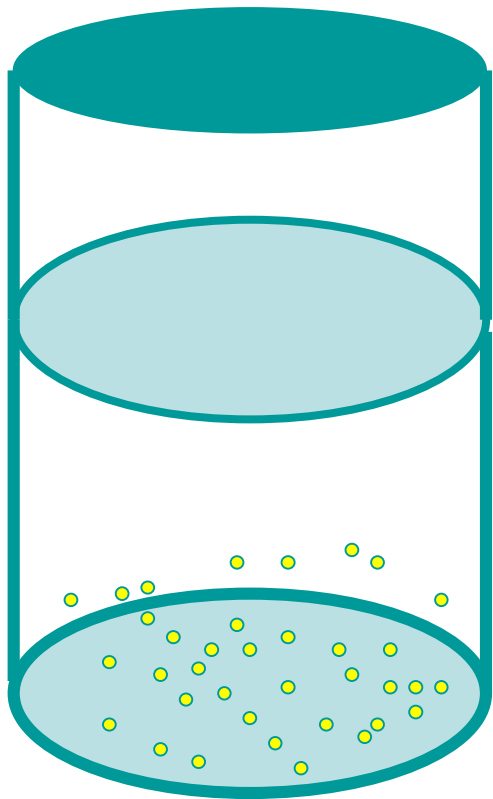
Substrato	Enzima	$k_{cat}/K_M$ ( $M^{-1}s^{-1}$ )	Stereoselettività ( $k_{cat}/K_M$ ) <sub>S</sub> / ( $k_{cat}/K_M$ ) <sub>R</sub>
(S)-fenilglicil↓OMe (R)-fenilglicil↓OMe	Penicillina amidasi da <i>E. coli</i>	550 1100	0.5
(S)-fenilglicil↓OMe (R)-fenilglicil↓OMe	α-Chimotripsina (bovino)	9.2 0.57	14
(S)-fenilglicil↓OMe (R)-fenilglicil↓OMe	Proteinasi K da <i>Tritirachium album</i>	0.6 0.3	2

Different hydrolases are able to hydrolyze the methyl ester of (R) and (S) phenylglycine but with different enantioselectivity

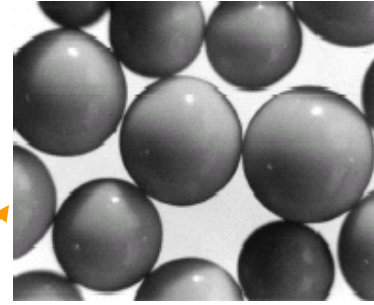
**The process:**  
**Biocatalysis in non conventional media**

# Biocatalysts in non-conventional media: multiphase systems

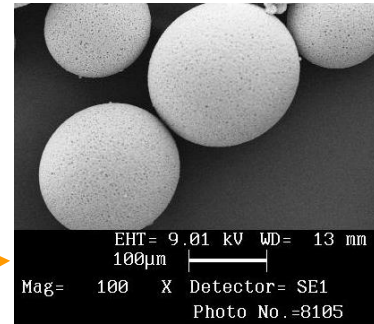
→ Anything different from a diluted aqueous solution



*Immobilized Enzymes working in buffer or org. solvent*



*Enzymes active on substrates anchored on solid phases*



*Enzymes (or cells) in low water media:*



**Organic solvent**  
**Neat substrates**  
**Water/organic solvent**  
**Ionic liquids**  
**Supercritical fluids**  
**Gases**

How to control, investigate and  
understand the  
physical-chemical phenomena  
in biocatalyzed systems



## How biocatalysts work under non-physiological conditions

**Neat  
substrates  
+  
Native  
enzyme  
+  
Traces of  
solvent**



**Neat  
substrates  
+  
Immobilized  
enzyme**

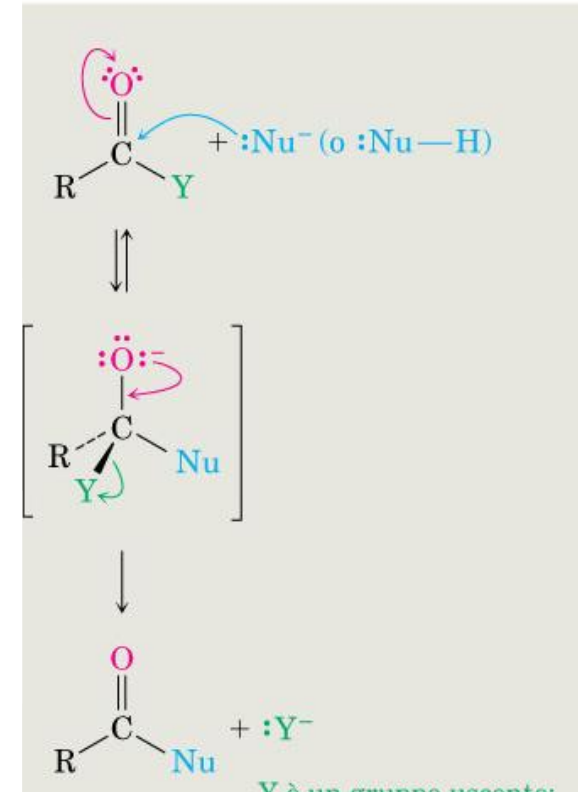
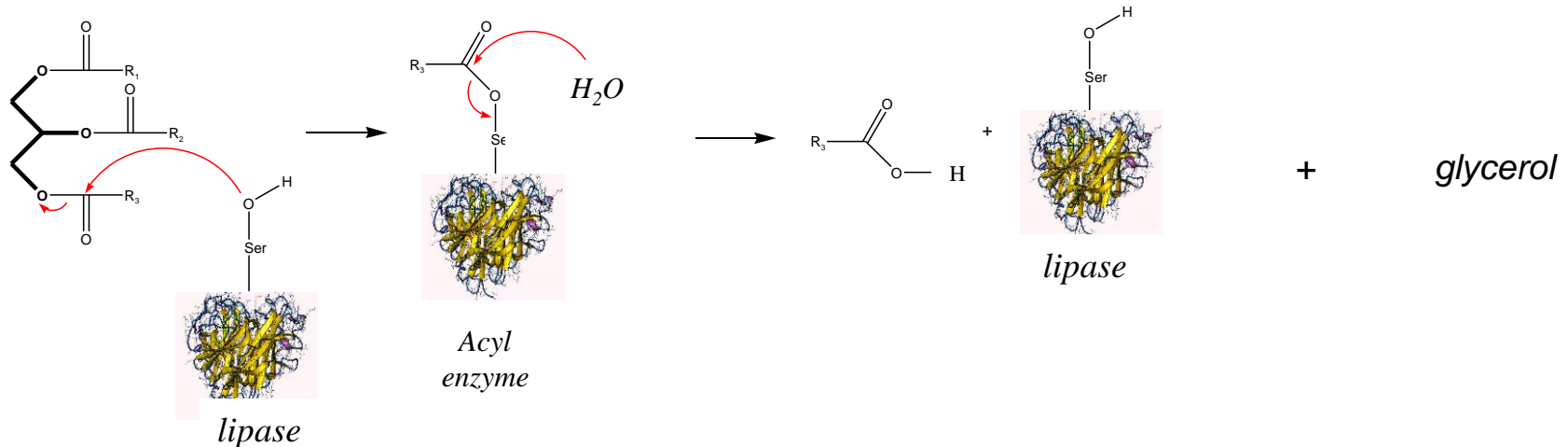


# Low-water media: advantages

- **Shift of thermodynamic equilibrium**
- **Recovery of products**
- **Solubility of hydrophobic substrates**
- **Microbial contamination negligible**
- **Side-reactions reduced**
- **Simple recycling of the catalyst**

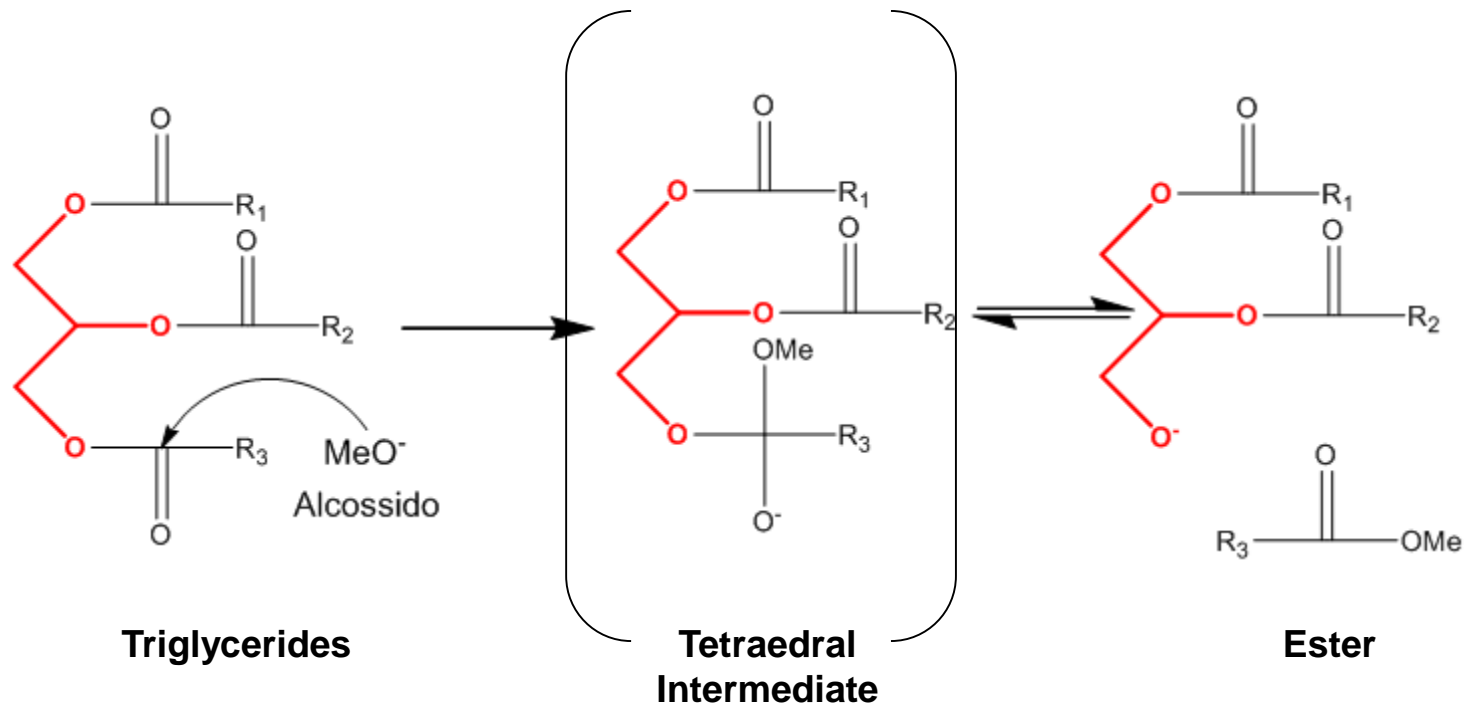
# Shifting the equilibrium towards the synthesis of acyl bond

Esterases  
Amidases  
Lipases  
Peptidases



# Chemical synthesis of biodiesel

*Alkaline or acid conditions*



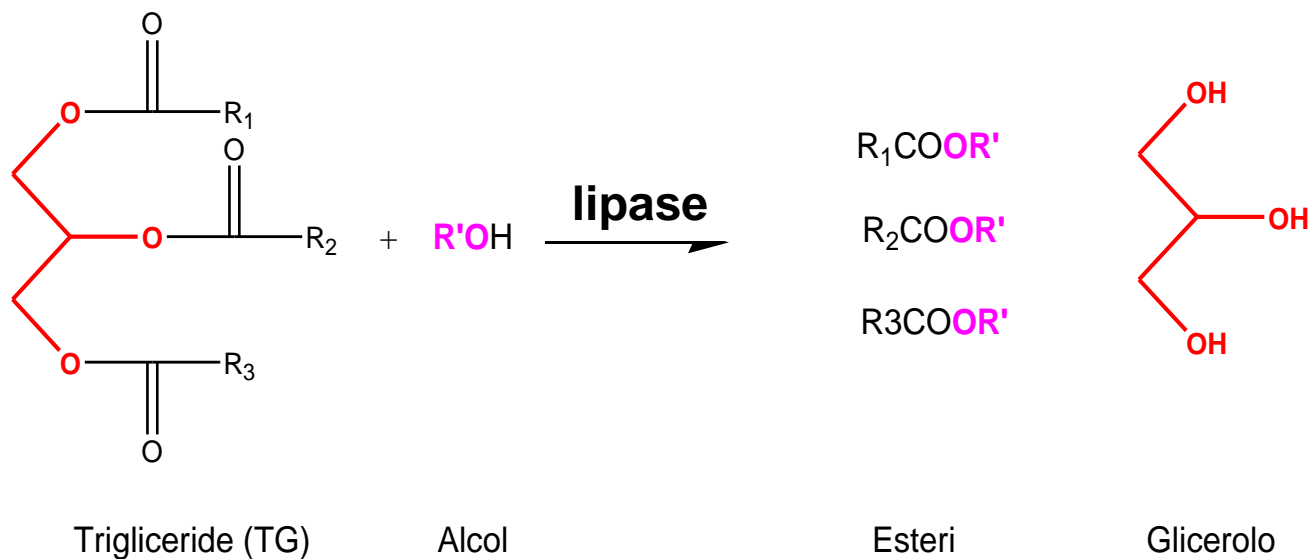
High temperatures

Separation of by product at the end of the processes (distillation)

Catalysts disposal

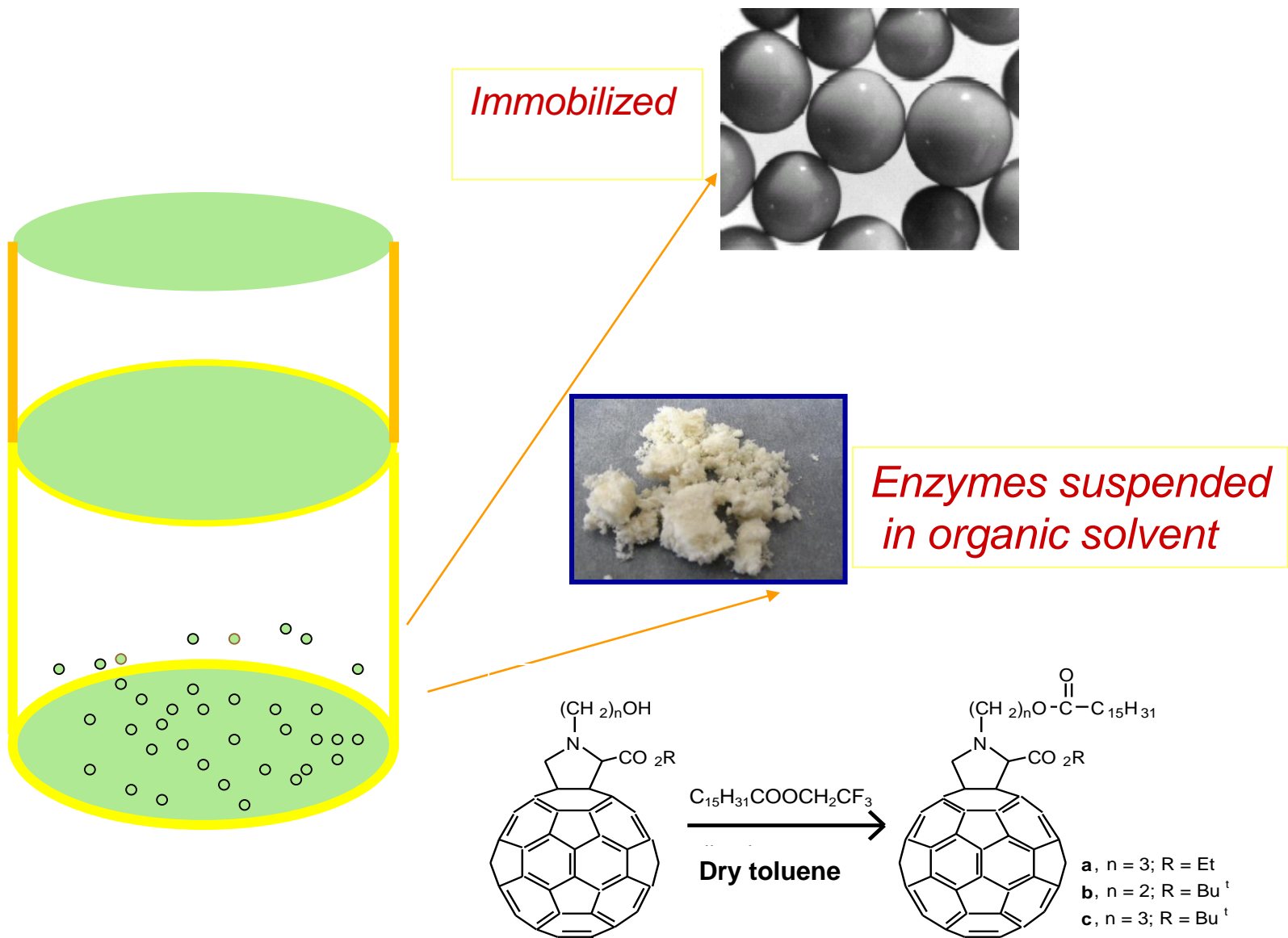
Low quality of glycerol

# Industrial examples: enzymatic esterification/transesterification of fats and oils



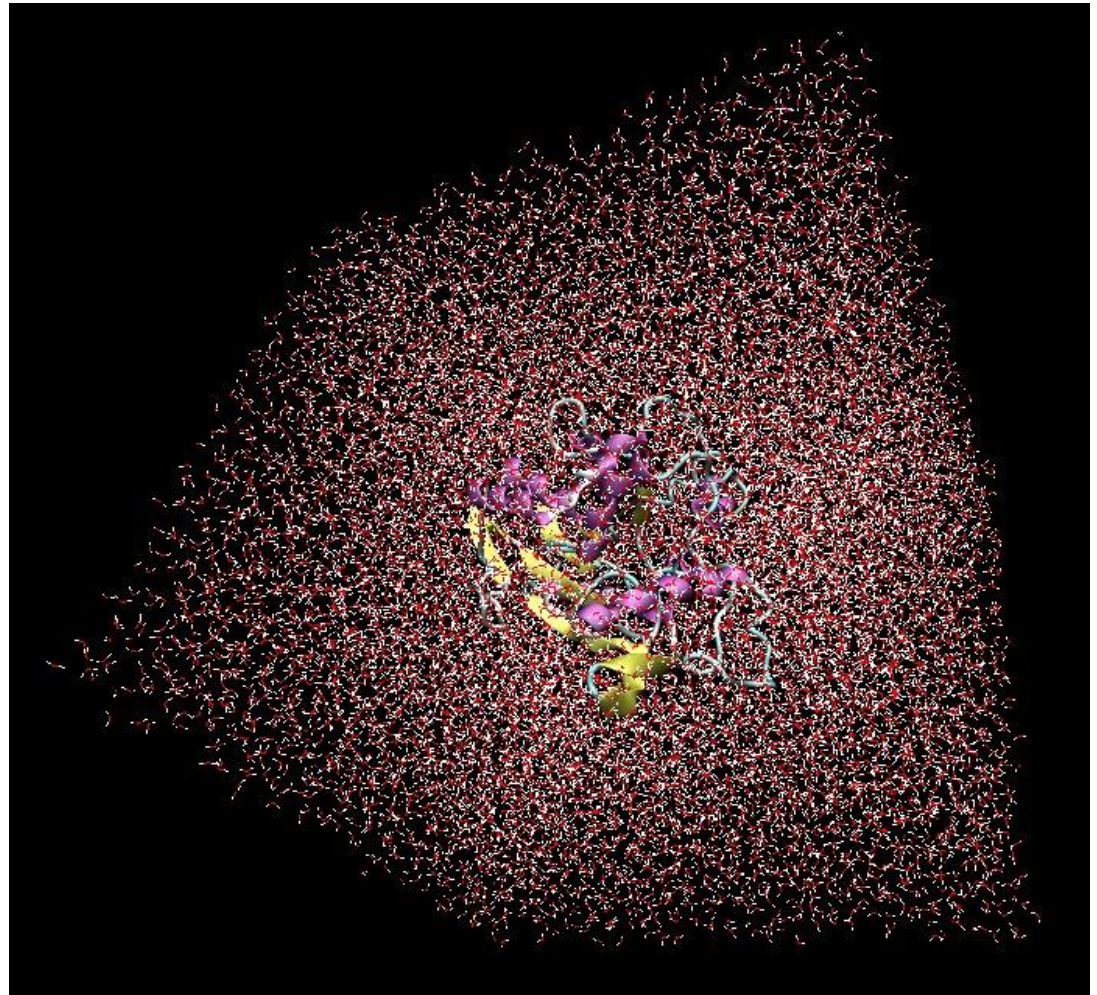
**Biodiesel**

# Low-water media: different systems



## Enzymes in aqueous medium: «close» to physiological environment

Surface water molecules are held to each other most strongly by the positively-charged basic amino acids. The exchange of surface water is controlled by the exposure of the groups to the bulk solvent .



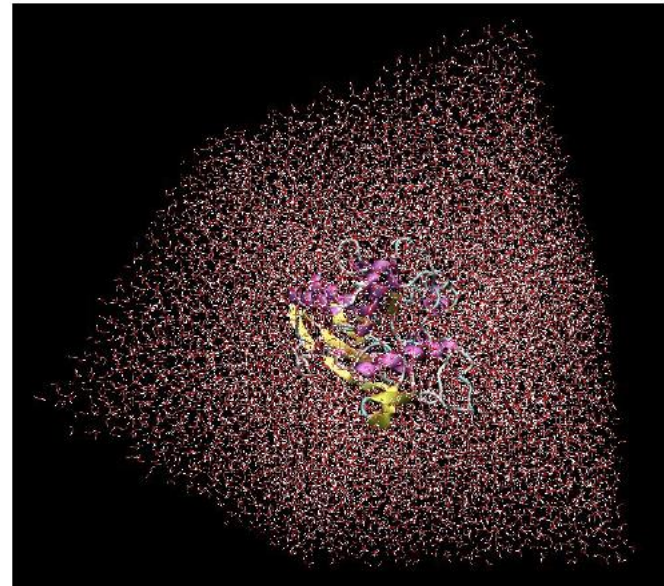
## The contribution of water to protein structure

Protein hydration is very important for their three-dimensional structure and activity. Indeed, **proteins lack activity in the absence of hydrating water.**

The aqueous structuring around proteins is affected out to at least **1 nanometer** from its surface.

In solution they possess a **conformational flexibility with** a wide range of **hydration states,**

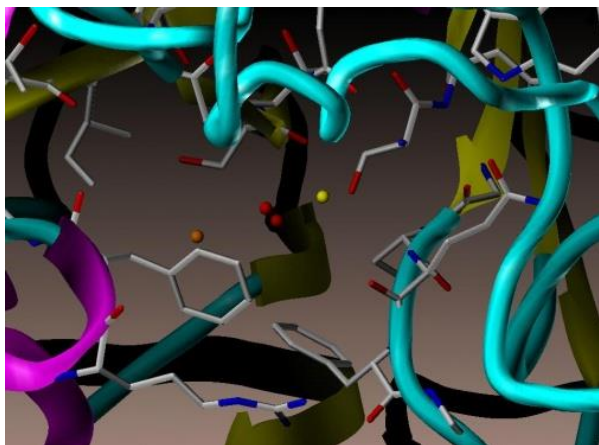
Equilibrium between these states will depend on the **activity of the water** ( $a_w$ ); that is, the freedom that the water has to hydrate the protein.



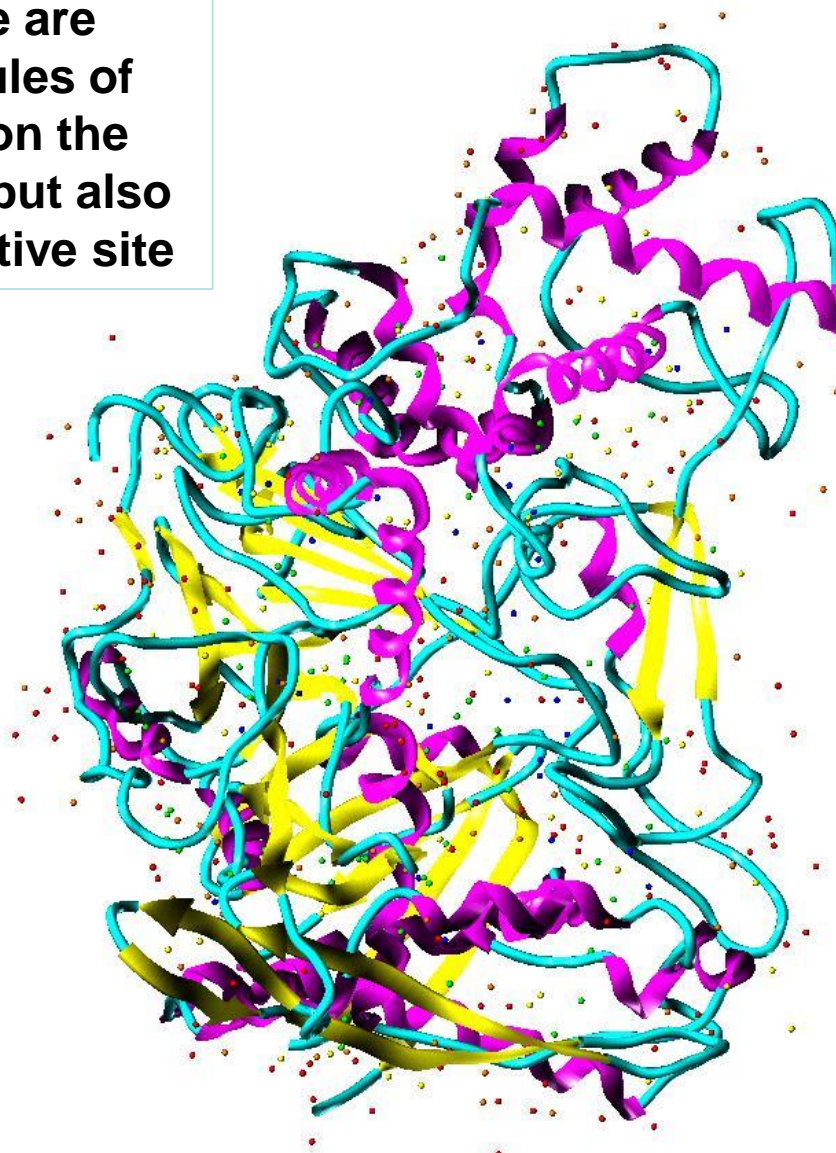


# Biocatalysts in organic solvents: residual water in PGA

Active site

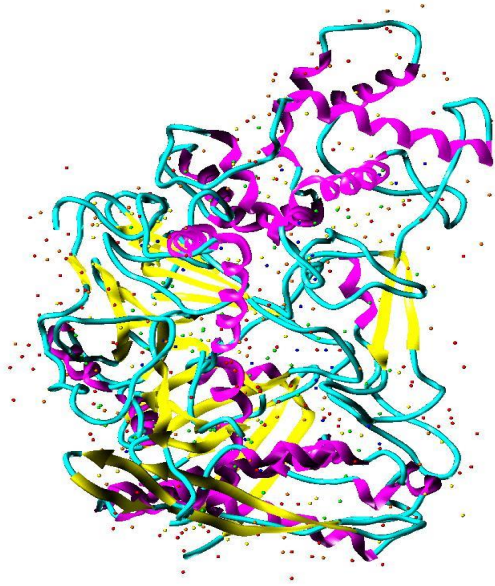


There are molecules of water on the surface but also in the active site



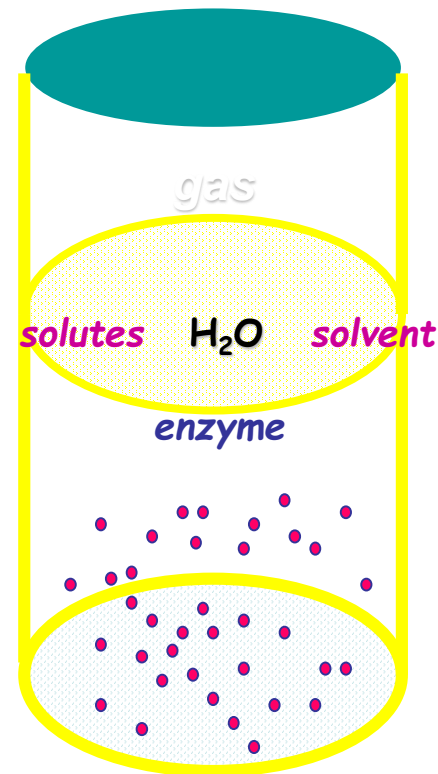
$\beta$   
Violet  
Blue  
Green  
Yellow  
Orange  
Red  
↓  
Strenght of bond

# Low water media: residual water and water activity ( $a_w$ )



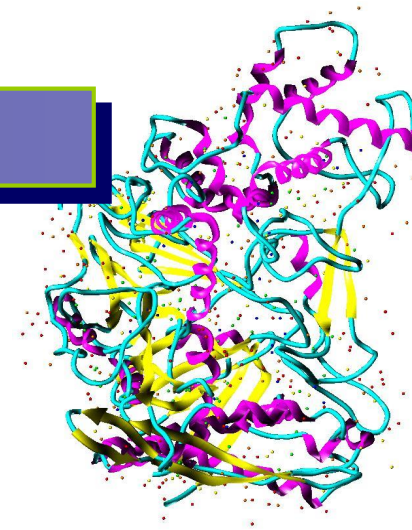
The concept of water activity can be assimilated to the “free” water present in the system, which is available to react or hydrate other molecules. When a system reaches the equilibrium, the water activity (or the “free water”) will be the same in all phases. Therefore, the reaction and the enzyme activity will be affected by the  $a_w$  rather than by the water concentration in the solvent.

➤ It is not sufficient to state the amount of added water



$a_w$

## Log P of organic solvents and effect on enzymatic activity

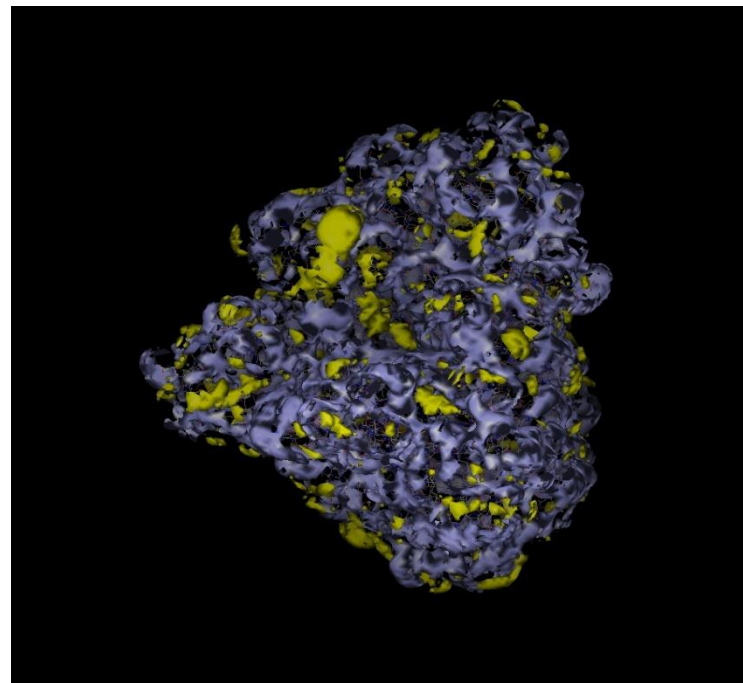
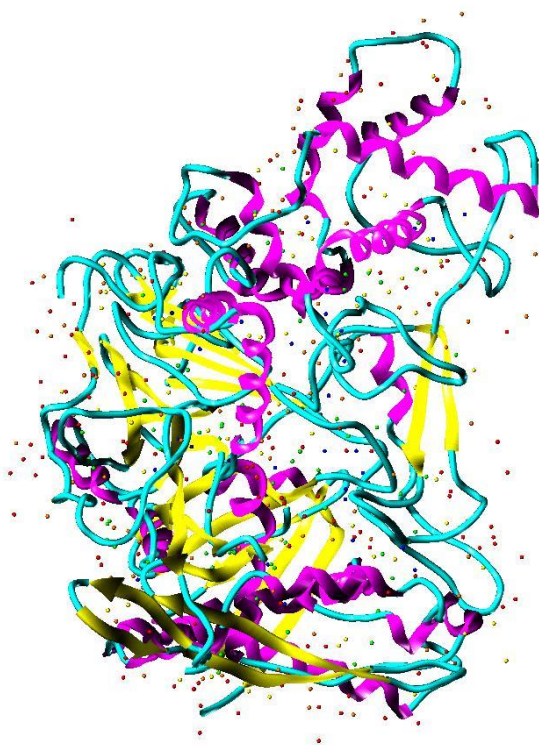


### Reaction media

- can compete for water molecules on the surface thus inducing denaturation
- can remove water molecules essential for the mechanism of action: enzyme retains its conformation but loses its activity

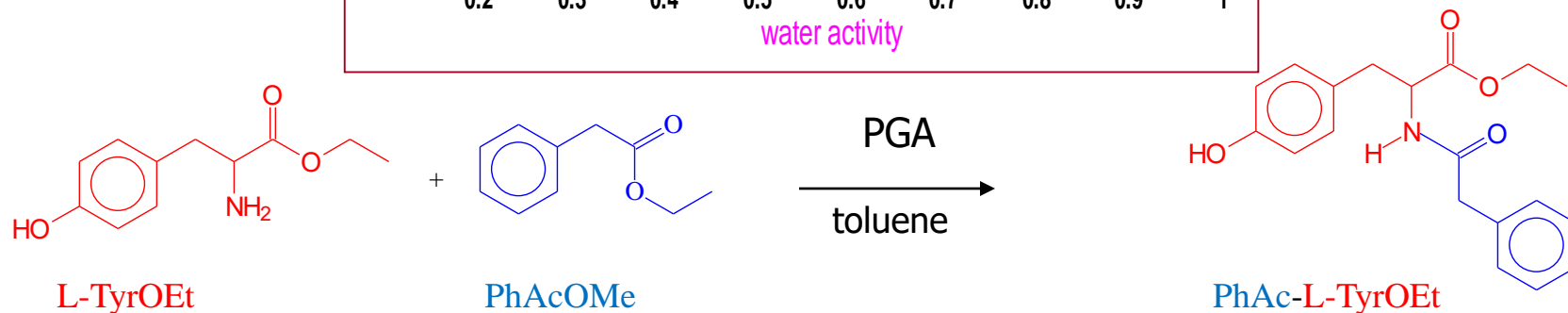
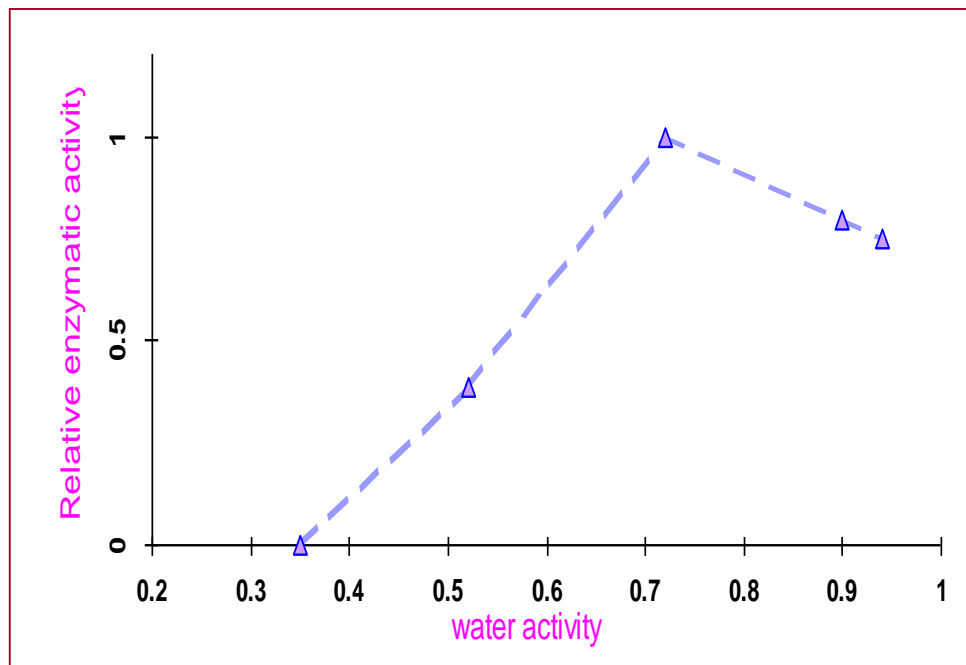
Log P	Water-Miscibility	Effects on enzyme activity
-2.5 to 0	Completely miscible	Used to solubilise lipophilic substrates in concentrations of 20-50% v/v without deactivating the enzyme
0 to 2	Partially miscible	Limited use due to rapid enzyme deactivation
2 to 4	Low miscibility	May be used with caution
> 4	Immiscible	<b>Ensures high retention of activity</b>

## Penicillin G amidase in organic solvent: active when sufficiently hydrated



The hydration of the biocatalyst will depend on the amount of “free water” (i.e. water activity) rather than on the amount of total water present in the system.

# $a_w$ effect on synthetic activity of PGA in organic solvent



Ebert, C.; Gardossi, L.; Linda, P., *Tetrahedron Lett.*, 1996, 37, 9377-9380

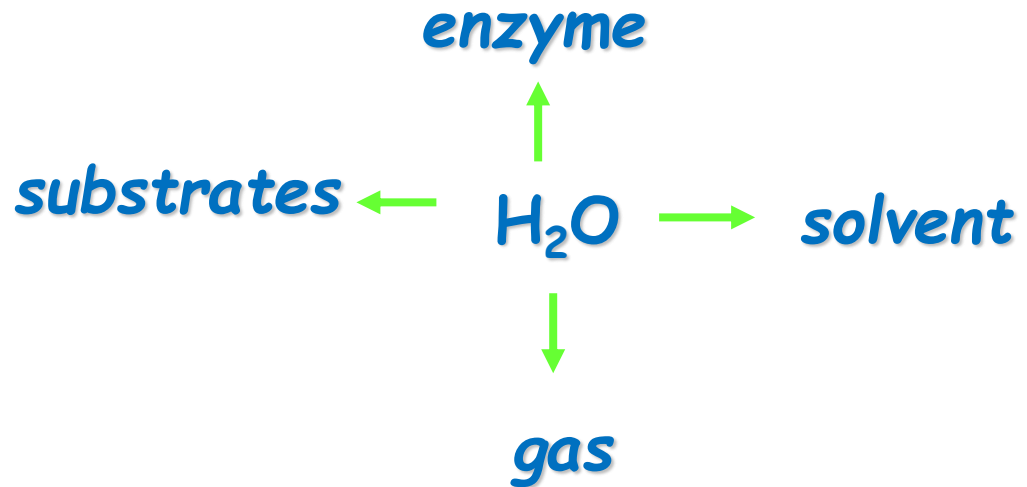
Ebert, C.; Gardossi, L.; Linda, P., *J. Mol. Catal. B*, 1998, 5, 241-244.

Basso A., De Martin L., Ebert C., Gardossi L., Linda P., Zlatev, V., *J. Mol. Catal. B*, 2001, 11, 851-855.



## How measuring or controlling the water activity

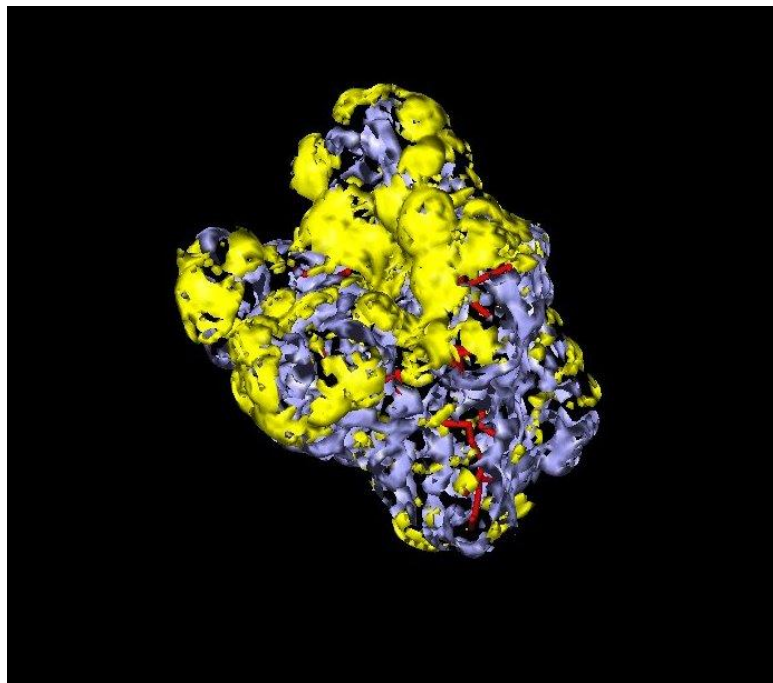
Since at the equilibrium the “free water” will be the same in all phases, it can be measured in the most accessible one, generally the gas phase *via* the measurement of vapour pressure of water.



- Evaluating water activity by measuring water pressure in the gas phase of the close system at the equilibrium
- Exploiting the ability of porous materials/carriers to control water distribution and mobility
- Drying or bring to a defined water content all ingredients/phases:  
By using pairs of hydrated salts “buffering” the  $a_w$

*Not all enzymes need the same amount of «free water»*

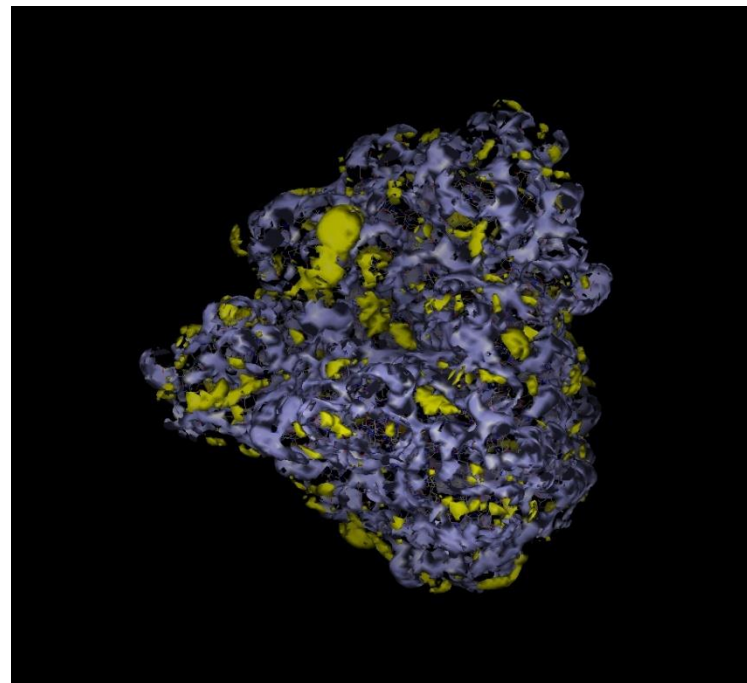
■ hydrophobic  
■ hydrophilic



**Lipase from *P. cepacia***



**Very active even at  
low water activity  
( $<0.2$ )**



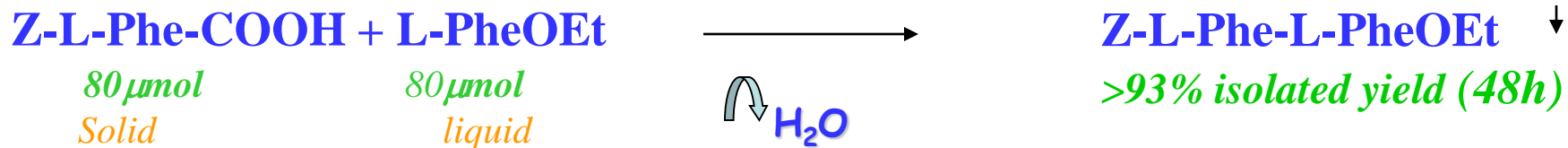
**(PGA) Amidase from *E. coli***



**Active only at water  
activity  $> 0.4$**

# Thermodynamically controlled synthesis with substrate suspension in toluene at controlled $a_w$

toluene (1mL),  $a_w=0.73$

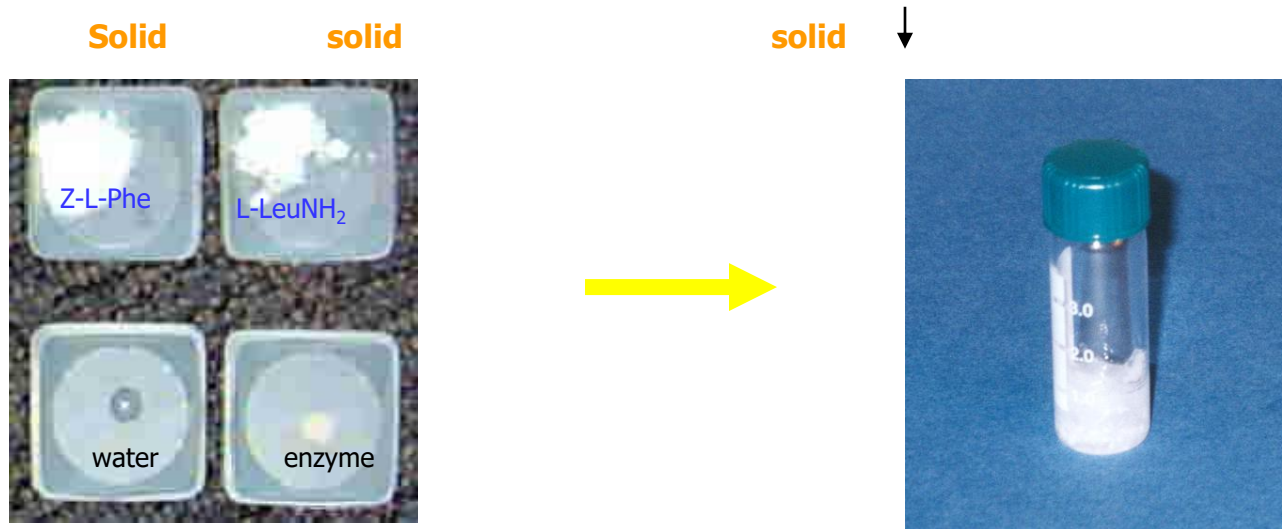
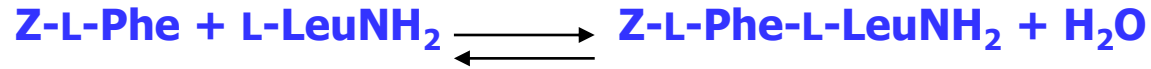


Enzyme	Acyl donor	Nucleophile	Conv. (%)	Time (h)
Thermolysin	Z-L-Phe-COOH	L-Phe-OEt (s)	<b>98</b> ↓	48
Thermolysin	Z-L-Phe-COOH	L-Tyr-OEt (s)	<b>97</b> ↓	144
Thermolysin	Z-L-Phe-COOH	L-Leu-NH <sub>2</sub> (s)	<b>95</b> ↓	96

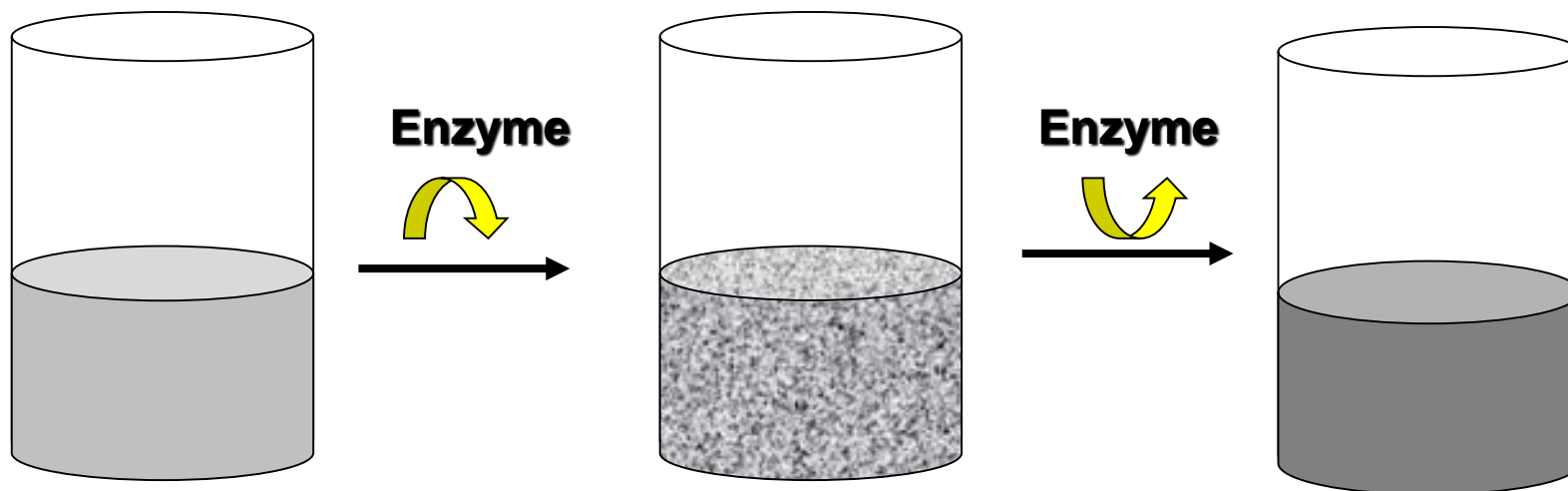


Some examples of even  
“more desperate “  
experimental conditions

# Precipitation driven “solid to solid” peptide synthesis: product solubility must be lower than substrate solubility



# *What is precipitation driven biocatalysis?*

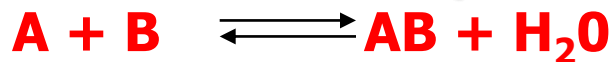


- **Solid Substrate + minimum Liquid Phase**
- **Solid Substrate and Product + Liquid Phase**
- **Solid Product + Liquid Phase**

**High volumetric productivity**

**The equilibrium lies completely either to the side of the solid substrate or to the side of the solid product**

# When is precipitation driven synthesis feasible? It depends on the thermodynamics of the reaction

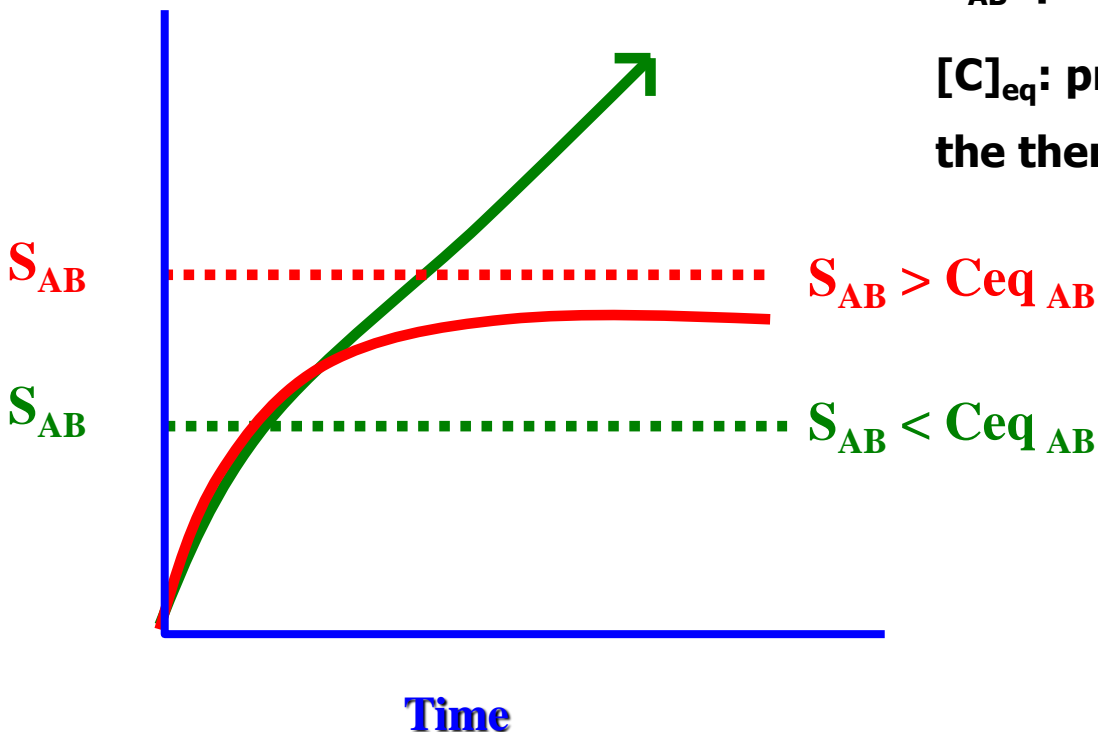


When:

•  $S_{AB} < [C]_{eq}$  the product precipitates and th. equilibrium is reached only when the substrate excess is completely consumed.

$S_{AB}$ : product solubility in the solvent;

$[C]_{eq}$ : product concentration in solution at the thermodynamic equilibrium



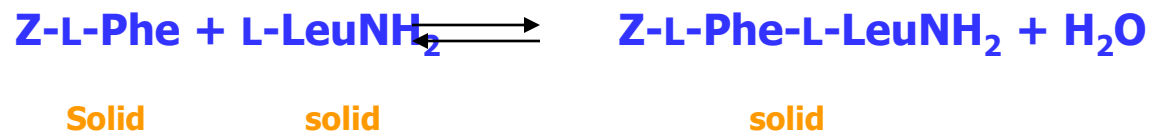
The feasibility  
is solvent  
INDEPENDENT

# Rules for Solvent Selection

- **The yield of crystalline product can be maximised by choosing a solvent where product solubility is lowest**
- **for hydrophobic targets water is generally a good choice**
- **in the synthesis of hydrophilic targets good yields are expected in hydrophobic solvents**

**Always use an excess of the most soluble compound**

# Thermodynamically controlled synthesis of Z-L-Phe-L-LeuNH<sub>2</sub> catalysed by Thermolysin in toluene

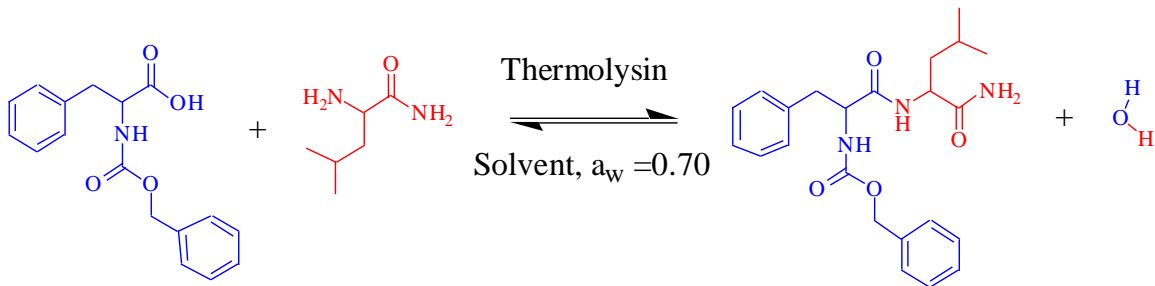


- ❖ 2 millimoles of Z-L-Phe and L-LeuNH<sub>2</sub> in 20mL toluene
- ❖ Conv. after 8h: > 99%
- ❖ 96% (1.92 millimoles) of pure solid product recovered by rinsing the enzymel
- ❖ Enzyme recycled 4 times

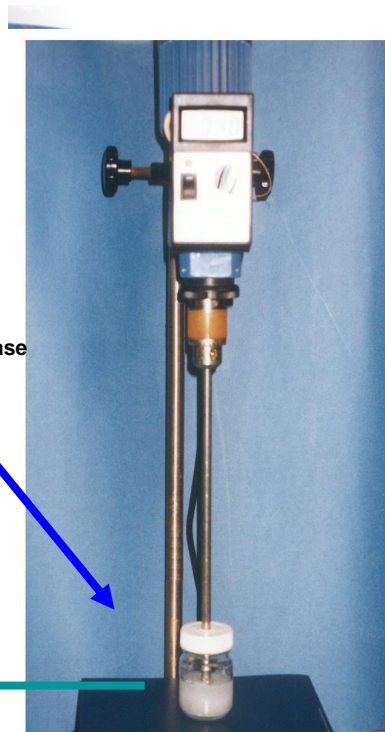
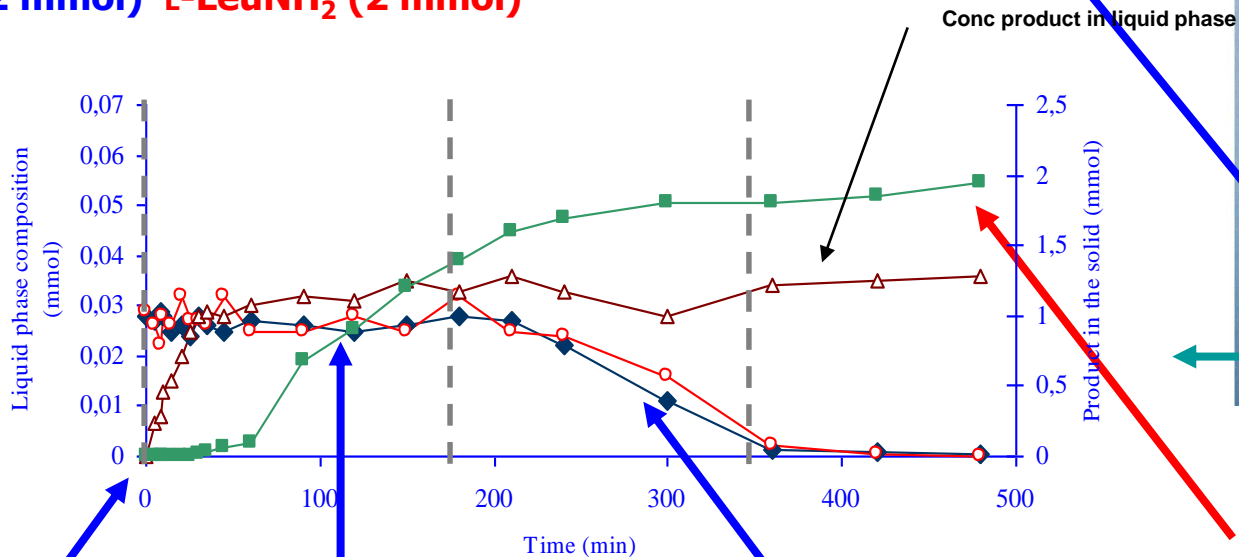
Mechanic stirrer



# How does it work?



**Z-L-Phe (2 mmol) L-LeuNH<sub>2</sub> (2 mmol)**



**- Conv. after 8 hours > 99%**  
**- 96% (1.92 millimol) of pure solid product at the equilibrium**

Product precipitation occurs when [ZPheLeuNH<sub>2</sub>] equals S<sub>ZPheLeuNH<sub>2</sub></sub>

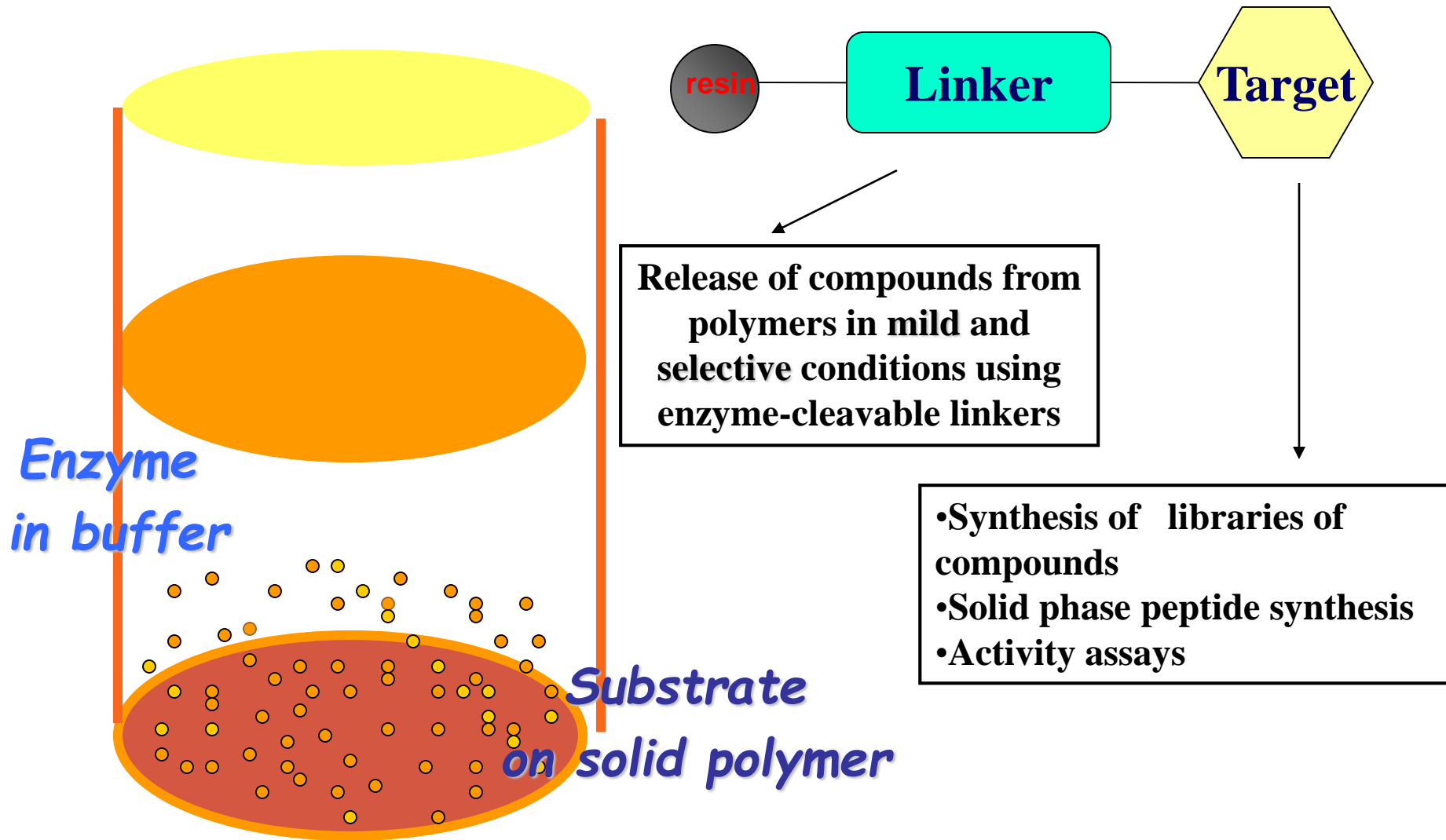
The solution phase reaches a steady state situation

-Substrates in solution reach the equilibrium concentration  
 -No more excess solid substrate is present

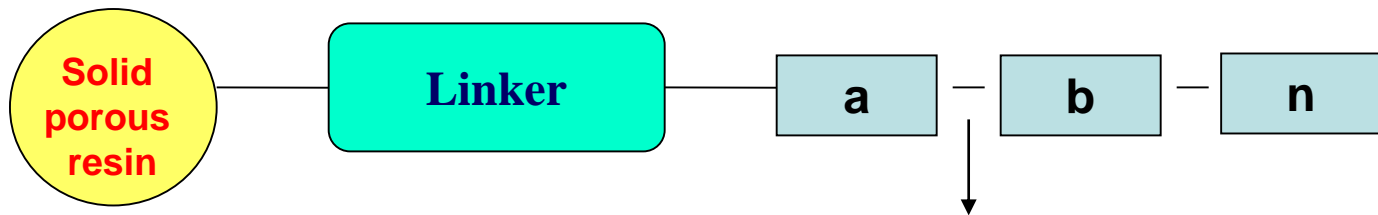
# Application of enzymes on solid substrates



# Solid phase biocatalysis



# Solid phase biocatalysis: peptide synthesis



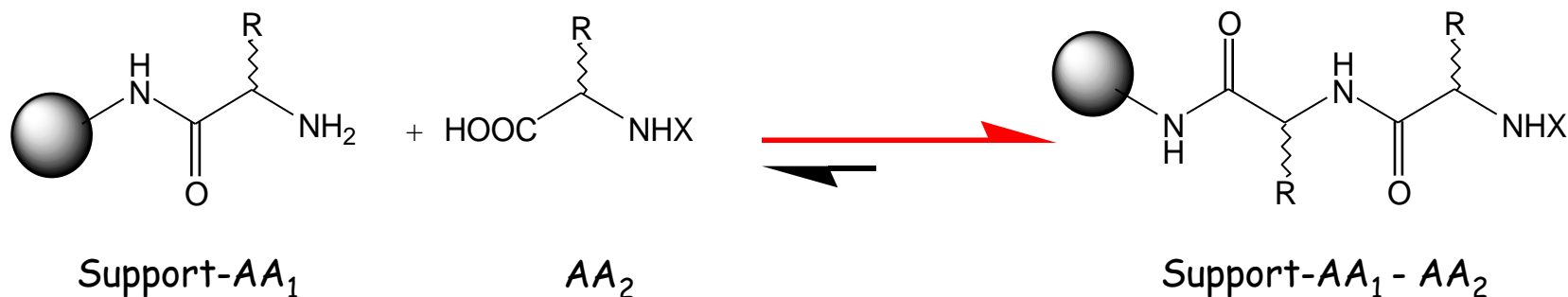
**Peptidases: enzymatic coupling**

## **Advantages:**

- **Minimal protection**
- **No racemization**
- **Equilibrium shifted to synthesis even in aqueous media**

# Solid phase biocatalysis: peptide synthesis

*Taking the advantages of organic solvent... in buffer*



- Suppressed ionisation of amino groups
- Solvation of hydrophobic substrates

# Annexes

## Equazione di Michaelis – Menten (1913)



Leonor Michaelis  
(1875–1949)

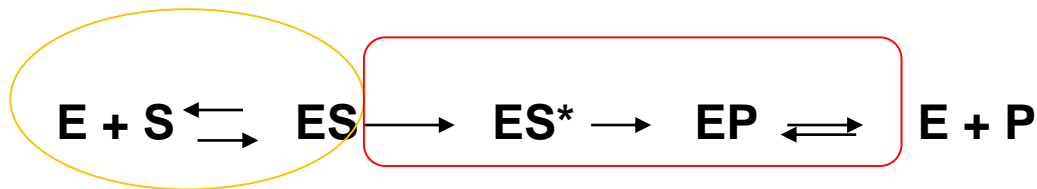
$$V = k_{\text{cat}} [E]_{\text{T}} \frac{[S]}{K_S + [S]}$$



Maud Leonora Menten  
(1879–1960)

oppure

$$v = V_{\text{max}} \frac{[S]}{K_M + [S]}$$

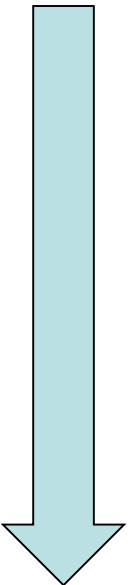
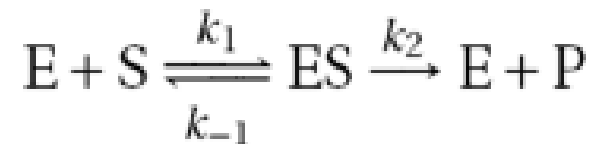


### Cinetica semplificata

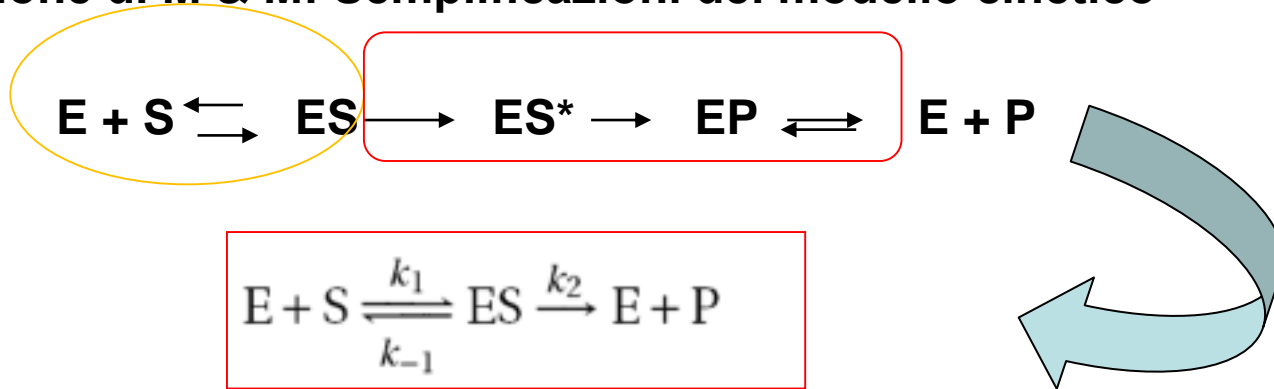
- Un enzima catalizza la reazione che dal substrato **S** porta al prodotto **P** attraverso il complesso enzima-substrato **ES** e il complesso enzima-prodotto **EP**:



- Si consideri la dissociazione di EP molto rapida e irreversibile; lo stadio successivo:



## L'equazione di M & M: Semplificazioni del modello cinetico



1. il primo stadio è rapido e reversibile, si forma il complesso enzima-substrato ES, la cui costante di dissociazione è  $K_s$ .

$$K_s = \frac{[E][S]}{[ES]}$$

2. Nel secondo stadio hanno luogo i processi chimici governati da una costante di velocità  $k_2 = k_{cat}$

$$V = k_2[ES] = k_{cat}[ES] = \frac{d[P]}{dt} = -\frac{dS}{dt}$$

## Come ricavare l'equazione di M & M

Scrivere il bilancio delle masse per ogni specie. Per l'enzima è:

$$[E]_T = [E]_{\text{lib}} + [ES]$$

$$[E]_{\text{lib}} = [E]_T - [ES]$$

$$K_S = \frac{[E][S]}{[ES]} = \frac{\{[E]_T - [ES]\}[S]}{[ES]}$$

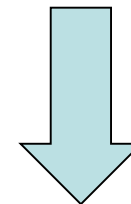
$$[ES]K_S = [E]_T[S] - [ES][S]$$

$$[ES]\{K_S + [S]\} = [E]_T[S]$$

$$[ES] = \frac{[E]_T[S]}{K_S + [S]}$$

$$V = k_2[ES] = k_{\text{cat}}[E]_T \frac{[S]}{K_S + [S]}$$

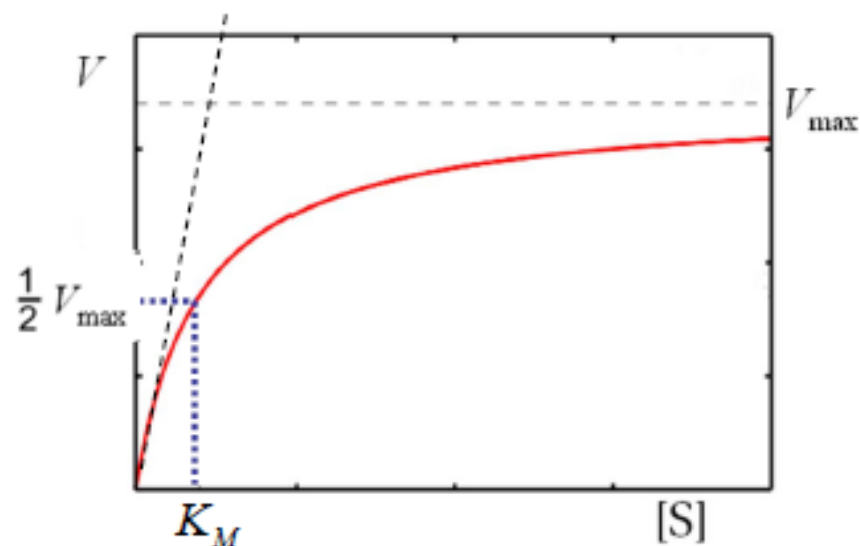
L'enzima non deve essere saturato dal substrato



□ Misurando  $V$  a diverse concentrazioni di  $S$  si trova la curva seguente:



$$V = k_{\text{cat}} [E]_{\text{T}} \frac{[S]}{K_S + [S]}$$



- Ad alte concentrazioni di S,  $K_S$  diventa trascurabile e  $V$  diventa:

$$V = \boxed{V_{\text{max}} = k_{\text{cat}} [E]_{\text{T}}} \quad \Rightarrow \quad V = V_{\text{max}} \frac{[S]}{K_S + [S]}$$

- Alla condizione nella quale  $V = \frac{V_{\text{max}}}{2} \Rightarrow V = \frac{V_{\text{max}}}{2} = \frac{V_{\text{max}} [S]}{K_S + [S]}$

$$[S] = K_S = K_M$$

costante di Michaelis – concentrazione del substrato necessaria a raggiungere una velocità pari a  $V = \frac{1}{2} V_{\text{max}}$

$$V = V_{\text{max}} \frac{[S]}{K_M + [S]}$$

equazione di Michaelis-Menten

## Significati di $K_M$

$$v = V_{\max} \frac{[S]}{K_M + [S]}$$

velocità è indipendente da [S].

- $[S] = K_M$      $V = V_{\max}/2$ , ossia
  - $K_M$  rappresenta la concentrazione di substrato che determina metà della velocità massima.
  - $K_M$  rappresenta pure la concentrazione di substrato alla quale metà dei siti attivi sono occupati, dando una misura della [S] richiesta affinché la catalisi avvenga in modo significativo
  - $K_M$  è una misura dell'energia di binding  $\Delta G_b$

$k_{\text{cat}}/k_m$  : specificity constant

$$v = V_{\text{max}} \frac{[S]}{K_M + [S]}$$

L'enzima non è saturato

- $[S] \ll K_M$  A concentrazioni molto basse di substrato, la velocità è direttamente proporzionale a  $[S]$ , infatti vale la relazione  $V = \frac{V_{\text{max}}}{K_M} [S]$
- $[S] \gg K_M$  A concentrazioni elevate di substrato,  $V = V_{\text{max}}$ , ossia la velocità è indipendente da  $[S]$ .

L'enzima è saturato

N.B.

La velocità che si misura è quella iniziale, quella relativa alla scomparsa del substrato o alla formazione del prodotto

$$V = \frac{d[P]}{dt} = -\frac{dS}{dt}$$

$K_{\text{cat}}/K_M$  va calcolata a basse concentrazioni di S, quando l'enzima non è saturo