

# Transfer function models

DINAMICA E CONTROLLO DEI PROCESSI CHIMICI  
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Corso di Laurea Magistrale in Ingegneria di Processo e dei Materiali



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## OBJECTIVE

- We would like to find a compact dynamic representation of the process, of the input-output type



$$Y(s) = G(s) \cdot U(s)$$

$$G(s) = \frac{Y(s)}{U(s)}$$

- We wish to represent the system in the Laplace domain, using a **transfer function G(s)**
  - It connects **one input**  $U(s)$  to **one output**  $Y(s)$
  - Input  $\leftrightarrow$  output
  - Forcing function  $\leftrightarrow$  response
  - Independent variable  $\leftrightarrow$  dependent variable
  - Cause  $\leftrightarrow$  effect
- It is expected that we have to transform the differential equations describing the system dynamics

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## EFFECT OF THE INITIAL CONDITIONS

- As an example, assume that a dynamic model is:

$$a_2 \frac{d^2 y(t)}{dt^2} + a_1 \frac{dy(t)}{dt} + a_0 y(t) = b \cdot u(t)$$

- $y(t)$  and  $u(t)$  are the output and the input, respectively
- $a_i$  and  $b$  are the model parameters (constant and known)

- Upon Laplace transformation:

$$a_2 \mathcal{L} \left[ \frac{d^2 y(t)}{dt^2} \right] + a_1 \mathcal{L} \left[ \frac{dy(t)}{dt} \right] + a_0 \mathcal{L}[y(t)] = b \mathcal{L}[u(t)]$$

- After algebraic manipulation:

$$Y(s) = \frac{b}{a_2 s^2 + a_1 s + a_0} U(s) + \frac{(a_2 s + a_1)y(0) + a_2 \dot{y}(0)}{a_2 s^2 + a_1 s + a_0}$$

Initial condition on the output  
 Initial condition on the derivative of the output

The final result depends on the initial conditions!

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## DEVIATION VARIABLES

- We have seen that when a time derivative (i.e., a differential equation) appears, the Laplace Transform results depends on the initial conditions on the output and on its derivative(s)
- Hence, given a differential equation, whatever the system initial conditions change, the resulting algebraic equation (in the Laplace domain) changes as well
- To avoid this inconvenience:
  - We assume that we are indeed studying the system dynamics, but the system is «started» from an initial steady-state condition → **the time derivatives of  $y(t)$  are null at  $t=0$**
  - The differential equations are written using «auxiliary» variables that represent the original ones, but are such that **auxiliary variable is null at time  $t=0$** 
    - Since a steady-state condition exists at  $t=0$ , we define these auxiliary variables as **deviation variables** (they deviate with respect to their initial steady-state values)
    - The prime symbol ( ' ) will be used to indicate a deviation variable (also called **perturbation variable**)

$$y' = y(t) - \bar{y}$$

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## DEVIATION VARIABLES

/cont'd

$$\begin{aligned} u'(t) &= u(t) - \bar{u} \\ y'(t) &= y(t) - \bar{y} \end{aligned}$$

where:

- $u'(t)$  and  $y'(t)$  are the deviation variables of  $u(t)$  and  $y(t)$ , respectively
- $\bar{u}$  and  $\bar{y}$  are the nominal steady-state values of  $u(t)$  and  $y(t)$ , respectively

■ It follows that:  $u'(0) = 0$ ;  $y'(0) = 0$

■ Additionally (same for  $u$ ):

$$\frac{dy'}{dt} = \frac{d(y - \bar{y})}{dt} = \frac{dy}{dt}$$

■ Hence, for  $t=0$ :

$$\left. \frac{dy'}{dt} \right|_{t=0} = 0$$

Notice: in this context, the prime symbol ( ' ) does **not** denote a first derivative!

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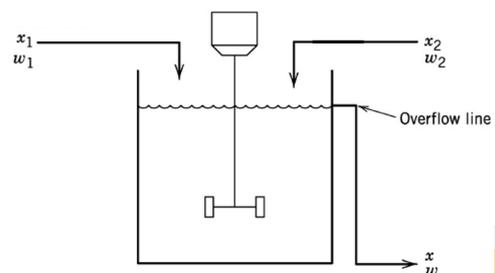


## TRANSFER FUNCTION DETERMINATION

- The transfer function (TF) we are looking for provides a link between the input and the output, when both are expressed in deviation variable form
  - It describes the dynamic behavior of the system when it moves away from the nominal steady state
  - This is exactly what one is interested to know from a process control perspective

■ Example:

- Derive the transfer function for a blender



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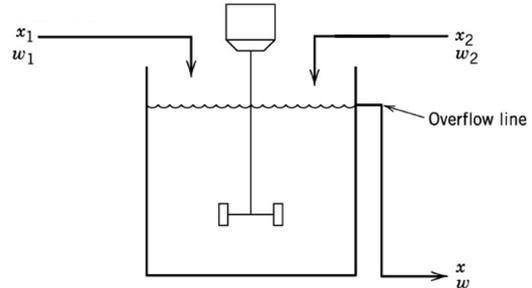
## SUMMARIZING THE EXAMPLE

- Perfect mixing of two liquid streams
  - ▷ Same solute A
  - ▷ Volume  $V = \text{const}$
  - ▷ Density  $\rho = \text{const}$
  - ▷ Mass flow rates  $w_1 = \text{const}$  and  $w_2 = \text{const}$

$$\rho V \frac{dx(t)}{dt} = w_1 x_1(t) + w_2 x_2(t) - w x(t)$$

- «General» case
  - ▷ Independent inputs are:  $x_1(t)$  and  $x_2(t)$
  - ▷ The output is:  $x(t)$

- We would like to show how, in the Laplace domain, the output depends on each of the inputs



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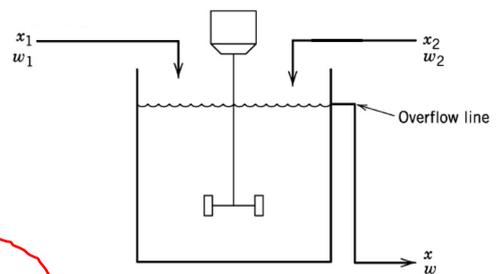
## EXAMPLE: DETERMINATION OF A TF

$$\left. \frac{X'(s)}{X_1'(s)} \right|_{x_2 = \text{const}} = G_1(s) = \frac{K_1}{\tau s + 1} \quad (\text{for } X_2'(s) = 0)$$

$$\left. \frac{X'(s)}{X_2'(s)} \right|_{x_1 = \text{const}} = G_2(s) = \frac{K_2}{\tau s + 1} \quad (\text{for } X_1'(s) = 0)$$

$$\tau = \frac{\rho V}{w}; \quad K_1 = \frac{w_1}{w}; \quad K_2 = \frac{w_2}{w}$$

- Two transfer functions are obtained
  - ▷ A variation in one independent input is «transferred» to the output through the TF related to that specific input
  - ▷ Each TF is called a «first-order» TF, because the polynomial in  $s$  appearing at the TF denominator is a first-order polynomial
- The knowledge of the initial conditions is not needed anymore!
  - ▷ Each TF provides a quantitative indication of how the output changes, with respect to its initial steady-state value, in response to a change of a given input (with respect to its initial steady-state value)



Independent inputs:  $x_1(t), x_2(t)$   
Dependent output:  $x(t)$

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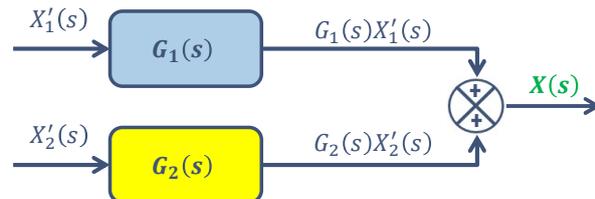


## THE SUPERPOSITION PRINCIPLE

- What happens if both inputs change simultaneously?
  - The Laplace transform is a linear operator

$$X'(s) = G_1(s)X_1'(s) + G_2(s)X_2'(s)$$

Block diagram representation



- The effects of the two inputs can be evaluated separately, and then they can be re-combined by simply summing them
  - **Additive property** of transfer functions (superposition principle)

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## USEFULNESS OF THE TRANSFER FUNCTION

- It completely characterizes the **input-output dynamics** of the system
- It allows knowing in detail **the system response** to any change of the **input**
  - It is **independent of the shape** of the input,  $U'(s)$ 
    - ❖ The TF is «normalized» with respect to the input
  - If **more** than one independent inputs exists, both the **single** effect and the **combined** effects can be described
- It is written in the terms of **deviation variables**
  - It does **not** depend on the initial conditions (provided that the system initial condition is a **steady-state** one)
  - Which initial steady state to start from does **not** influence the final result (provided that the system is a **linear** one)
- Notice
  - In the following, we will **always** assume that **TFs are written in deviation variable form**
  - We will usually **not** use the prime symbol ( ' ) to indicate a deviation variable

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## THE STEADY-STATE GAIN

### ■ Steady-state gain K

- ▷ It is the ratio between two changes, both calculated with respect to two steady-state conditions (steady-state ① and steady-state ②)

$$K = \frac{\text{output change following an input change}(1 \rightarrow 2)}{\text{input change}(1 \rightarrow 2)} = \frac{\bar{y}_2 - \bar{y}_1}{\bar{u}_2 - \bar{u}_1}$$

### ■ In truly linear systems:

- ▷ The gain value does **not** depend on the reference **steady state**
- ▷ The gain value does **not** depend on **the amplitude of the input perturbation**

### ■ The perturbation «shape» is not important

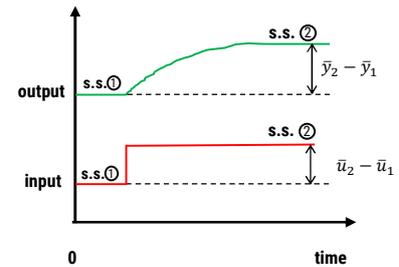
- ▷ What matters is that the **input** eventually reaches a **steady-state value**
- ▷ Usually, a **step** change is used

### ■ A distinct gain exists for **each input-output pair**

- ▷ But **not all** real systems have a steady-state gain!

### ■ Each steady-state gain has its **own measurement units** (output u.m./input u.m.)

- ▷ And its value can be **positive** or **negative**



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## THE CALCULATION OF THE STEADY-STATE GAIN

### ■ If the TF of a system is known, determining its gain is simple:

$$K = \frac{\bar{y}_2 - \bar{y}_1}{\bar{u}_2 - \bar{u}_1}; \quad G(s) = \frac{Y(s)}{U(s)}$$

**To find the steady-state gain (if it exists) with respect to a given input, one only needs to evaluate the relevant TF @ s=0:  $K = G(0)$**

- ▷ Assume a unit step change of input u
  - ❖ Hence, the denominator in the K expression is 1 (with own units)
- ▷ It follows that  $U(s) = \frac{1}{s} \rightarrow Y(s) = G(s) \cdot U(s) = \frac{1}{s} G(s)$
- ▷ We are interested at the steady-state change in y; in terms of deviation variables (with respect to the starting steady-state 1), it follows that:

$$K = \frac{\bar{y}_2 - \bar{y}_1}{1} \rightarrow K = \bar{y}_2 - \bar{y}_1 = y'(t) \Big|_{s,s} = \lim_{t \rightarrow \infty} y'(t)$$

- ▷ Final value theorem:  $\lim_{t \rightarrow \infty} y'(t) = \lim_{s \rightarrow 0} [sY(s)] \rightarrow K = \lim_{s \rightarrow 0} G(s)$

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## ORDER OF DYNAMIC SYSTEMS

- Let's consider a generic dynamic system:

$$a_n \frac{d^n y(t)}{dt^n} + a_{n-1} \frac{d^{n-1} y(t)}{dt^{n-1}} + \dots + a_1 \frac{dy(t)}{dt} + a_0 y(t) = b_m \frac{d^m u(t)}{dt^m} + b_{m-1} \frac{d^{m-1} u(t)}{dt^{m-1}} + \dots + b_1 \frac{du(t)}{dt} + b_0 u(t)$$

- Upon Laplace transformation it follows that:

$$G(s) = \frac{Y(s)}{U(s)} = \frac{b_m s^m + b_{m-1} s^{m-1} + \dots + b_0}{a_n s^n + a_{n-1} s^{n-1} + \dots + a_0}$$

Notice the order of numerator and denominator

- The TF appears (in deviation variable form) as a ratio of two polynomials (of different orders) in  $s$
- The **order of the dynamic system** is the degree ( $n$ ) of the **denominator** polynomial
  - The **relative order** (or relative degree) of the system is the difference ( $n-m$ )
  - Roots of the **denominator** polynomial are called **poles**
  - Roots of the **numerator** polynomial are called **zeroes**
- The steady-state **gain** of  $G(s)$  is equal to  $b_0/a_0$ 
  - Simply set  $s=0$  on the  $G(s)$  expression

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## CHARACTERISTIC POLYNOMIAL

$$G(s) = \frac{Y(s)}{U(s)} = \frac{b_m s^m + b_{m-1} s^{m-1} + \dots + b_0}{a_n s^n + a_{n-1} s^{n-1} + \dots + a_0}$$

- By dividing both the numerator and the denominator by  $a_0$ , the system **characteristic polynomial** is obtained at the denominator
    - It can be factored as the product of a sequence:  $\prod_i (\tau_i s + 1)$
- $$G(s) = \frac{Y(s)}{U(s)} = \frac{KB(s)}{(\tau_1 s + 1)(\tau_2 s + 1) \dots (\tau_n s + 1)}$$
- The  $B(s)$  polynomial has order  $m$
  - This form of  $G(s)$  is called «Time constant form»
    - It highlights the **individual time constants**  $\tau_i$  that determine the dynamic response of the system
      - Strictly speaking,  $\tau_i$  is called «time constant» only if it is real and positive; on a general basis,  $\tau_i$  might be negative or complex
    - Inspection of the individual  $\tau_i$  provides information about the **speed** and the **shape** of the dynamic response, as we will see later during this course

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## A PROPERTY OF TFs

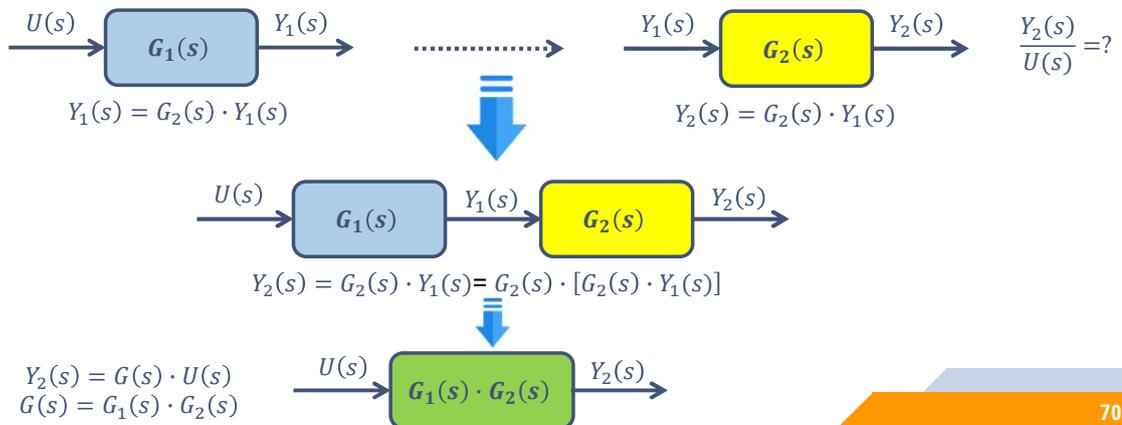
$$G(s) = \frac{Y(s)}{U(s)} = \frac{b_m s^m + b_{m-1} s^{m-1} + \dots + b_0}{a_n s^n + a_{n-1} s^{n-1} + \dots + a_0}$$

- In **real** («physical») dynamic systems, **n ≥ m** always results
  - ▷ **Physical realizability** condition.
- Why does this hold true in a real physical system?
  - ▷ If  $m > n$  were possible, then, for example, the following would be possible:  $a_0 y = b_1 \frac{du}{dt} + b_0 u$  ( $n=0; m=1 > n$ )
  - ▷ A step change in  $u$  (e.g., a valve is suddenly opened) would result in an **impulse** change in  $y$  (i.e.,  $y$  would change infinitely fast as the step occurs:  $\frac{du}{dt} \rightarrow \infty$ )
  - ▷ This is usually **impossible** to achieve in real systems
  - ▷ Every real system responds with «inertia» to any input change («at most»,  $n=m$  may be found)
    - ❖ The **relative order** quantifies the **degree of inertia** of an output with respect to an input change
  - ▷ Few exceptions exists (e.g., explosions!!!!)
- When  $m > 0$  is found, the system is said to have numerator dynamics
  - ▷ This means that a polynomial of degree at least 1 appears as the TF numerator



## ONE MORE PROPERTY OF TFs

- Besides the additive property, TFs also have a **multiplicative** property





## QUESTIONS

1. How does the value of K change, if the forcing function changes?
2. Can you think of a real case when it is not possible to identify the gain?
3. How will the output appear, if the K value is negative?
4. Can you make an example of a case where the K value is negative?
5. Suppose you are an operator, responsible for the performance of a chemical process. Your boss asks you to evaluate the gain of a dynamic control system using a step forcing function. Will you use a high or a low amplitude?
6. Would you rather have a high or a low time constant for a chemical reactor? Consider different point of view.

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## LINEAR SYSTEMS AND NONLINEAR SYSTEMS

- The Laplace transformation can be applied only to a linear differential equations with constant coefficients (linear systems)

$$a_n \frac{d^n y(t)}{dt^n} + a_{n-1} \frac{d^{n-1} y(t)}{dt^{n-1}} + \dots + a_1 \frac{dy(t)}{dt} + a_0 y(t) = b_m \frac{d^m u(t)}{dt^m} + b_{m-1} \frac{d^{m-1} u(t)}{dt^{m-1}} + \dots + b_1 \frac{du(t)}{dt} + b_0 u(t)$$

- ▷ The output dynamics (i.e., the y derivatives) depends linearly on the output itself, on the input u and on the input derivatives

- What does «linear system» mean on a physical basis?

1. For a linear system, the **superposition principle** holds true

$$u_1(t) \rightarrow y_1(t)$$

$$\rightarrow (u_1 + u_2) \rightarrow (y_1 + y_2)$$

$$u_2(t) \rightarrow y_2(t)$$

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## LINEAR SYSTEMS AND NONLINEAR SYSTEMS /cont'd

2. The dynamic response is **independent** of the operating conditions

input  $\Delta u_1 = \Delta u_2$

input  $\Delta u_1 = -\Delta u_2$

output  $\Delta y_1 = \Delta y_2$

output  $\Delta y_1 = -\Delta y_2$

input  $\Delta u_1 = 2\Delta u_2$

output  $\Delta y_1 = 2\Delta y_2$

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## NONLINEAR SYSTEMS

- It is very uncommon (actually, never) that a real process appears linear:  $\frac{a_1}{a_0} \frac{dy(t)}{dt} + y(t) = \frac{b_0}{a_0} u(t)$ 
  - ▷ Usually, the dynamic response is represented by:  $\frac{dy(t)}{dt} = f[y(t); u(t)]$

where function  $f$  include terms that are nonlinear with respect to the output  $y$  and/or to the independent input  $u$  (and possibly to the derivatives of  $u$ )

- ▷ Examples of nonlinearity related to typical outputs (temperature  $T$  and composition  $x$ )
  - ❖ A kinetic constant  $k$  depends on temperature  $T$  in a nonlinear way:  $k = g[T(t)] = k_0 e^{\frac{E_a}{RT(t)}}$
  - ❖ Vapor pressure  $P^{sat}$  depends on temperature  $T$  in a nonlinear way:  $P^{sat} = g[T(t)] = \exp\left(A - \frac{B}{T(t)+c}\right)$
  - ❖ The vapor-phase equilibrium composition  $y^*$  depends on the liquid-phase composition in a nonlinear way even for trivial ideal systems:

$$y^* = g[x(t)] = \frac{\alpha x(t)}{1 + (\alpha - 1)x(t)}$$

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## NONLINEAR SYSTEMS

It is very uncommon (actually, never) that a real process appears linear:  $\frac{a_1}{a_0} \frac{dy(t)}{dt} + y(t) = \frac{b_0}{a_0} u(t)$

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where function f include terms that are nonlinear with respect to the output y and/or to the independent input u (and possibly to the derivatives of u)

Examples of nonlinearity related to typical outputs (temperature T and composition x)

- ❖ A kinetic constant k depends on temperature T in a nonlinear way:  $k = g[T(t) = k_0 e^{\frac{E_a}{RT(t)}}$
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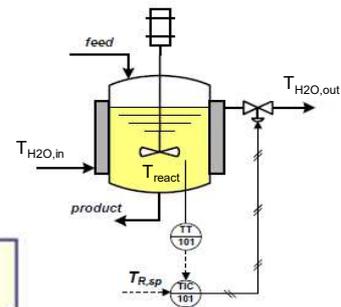
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## AN EXAMPLE OF A NONLINEAR RESPONSE

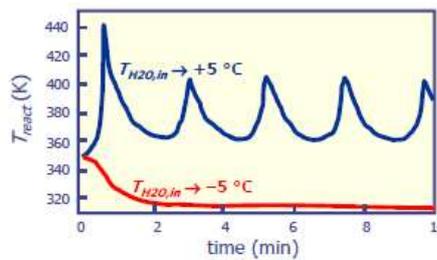
A jacketed CSTR, wherein a first-order exothermic irreversible reaction occurs:  $A \rightarrow B, \Delta H_r < 0$

Response of  $y=T_{react}$  to symmetric (increase/decrease) step changes on  $u=T_{H2O,in}$



**The response is strongly nonlinear!!!**

- ❖ The nonlinearity extent depends on the reaction kinetics, operating conditions, reactor geometry
- ❖ The system gain (and time constant) significantly change with operating conditions



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## LAPLACE TRANSFORM & NONLINEAR SYSTEMS

### Example

- > Linear system:  $\frac{dy'(t)}{dt} = ay'(t) + bu'(t)$   
 $\rightarrow \mathcal{L}\left[\frac{dy'(t)}{dt}\right] = \mathcal{L}[ay'(t) + bu'(t)] = \mathcal{L}[ay'(t)] + \mathcal{L}[bu'(t)] = aY'(s) + bU'(s)$
- > Nonlinear system:  $\frac{dy'(t)}{dt} = ay'(t)u'(t)$  this product gives rise to a nonlinear term  
 $\rightarrow \mathcal{L}\left[\frac{dy'(t)}{dt}\right] = \mathcal{L}[ay'(t)u'(t)] \neq \mathcal{L}[ay'(t)] \cdot \mathcal{L}[u'(t)] = \text{????}$

**The Laplace Transform cannot be calculated for nonlinear terms!!!**

How to determine the TF of a nonlinear system?



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## LINEARIZATION OF NONLINEAR SYSTEMS

$$\frac{dy(t)}{dt} = f[y(t); u(t)]$$

- To be able to determine the TF for these systems, one needs to approximate  $f(y,u)$  with a linear expression
  - > A Taylor series approximation around a nominal steady state is done, truncating it to the 1° order terms

$$f[y(t); u(t)] \cong f(\bar{y}; \bar{u}) + \left. \frac{\partial f}{\partial y} \right|_{\bar{y}; \bar{u}} \cdot (y - \bar{y}) + \left. \frac{\partial f}{\partial u} \right|_{\bar{y}; \bar{u}} \cdot (u - \bar{u})$$

- > At steady state, we have:  $f(\bar{y}; \bar{u}) = 0$
- > By using deviation variables  $y'$  and  $u'$  we obtain:

$$\frac{dy'}{dt} \cong \left. \frac{\partial f}{\partial y} \right|_{s.s.} \cdot y' + \left. \frac{\partial f}{\partial u} \right|_{s.s.} \cdot u'$$

Both  $y'$  and  $u'$  now appears as summation terms, i.e. **linearly!!!**  
(s.s.=nominal steady state)

- > This operation is called system **linearization**.  
It must be extended to **all independent input** and **all outputs** appearing in  $f$

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## INTERPRETING THE LINEARIZATION

$$\frac{dy(t)}{dt} = f[y(t); u(t)]$$

- Simple example:

$$\frac{dy(t)}{dt} = f[y(t)] \rightarrow \frac{dy'}{dt} \cong \left. \frac{\partial f}{\partial y} \right|_{\bar{y}} y'$$

- The parameters (gain, time constant) of the TF obtained after linearization are affected by the slope of function  $f$ , not by the value of  $f$  itself
  - ▷ The slope changes with the linearization point
  - ▷ **For nonlinear systems, the gain and the time constant depend on the nominal steady state!**
- If the actual conditions are not far from the nominal steady-state ones (i.e., if  $y(t) \cong \bar{y}$ ), the linear approximation is usually **satisfactory** for a real system

