


Modello atmosfera isoterma

$$\frac{dP}{dy} = -\rho g = -\frac{PM_A}{RT} g = -\frac{M_A g}{RT} P \Rightarrow$$

$y \uparrow$    $\rho = \rho(y)$   
 $PV = nRT$

separazione delle variabili

$$\frac{dP}{P} = -\frac{M_A g}{RT} dz \Rightarrow \int_{P_i}^{P_f} \frac{dP}{P} = -\frac{M_A g}{RT} \int_{z_i}^{z_f} dz \rightarrow \int_{P_0}^P \frac{dP'}{P'} = \dots$$

$$\ln \frac{P_f}{P_i} = -\frac{M_A g}{RT} (z_f - z_i)$$

$$\frac{P_f}{P_i} = \exp \left[ -\frac{M_A g}{RT} (z_f - z_i) \right]$$

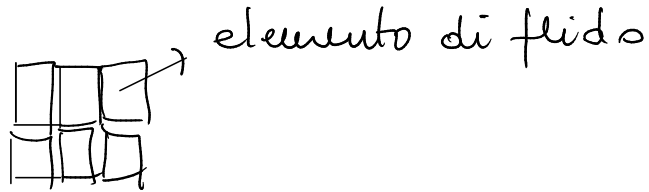
$$P_f = P_i \exp \left[ -\frac{z_f - z_i}{L} \right]$$

$$P = P_0 \exp \left[ -\frac{z - z_0}{L} \right]$$

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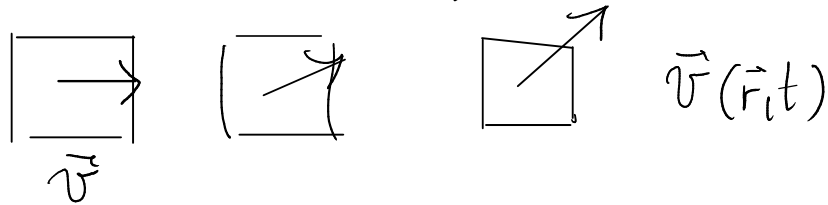
# DINAMICA DEI FLUIDI

- fluidodinamica: fluidi comprimibili HARD
- idrodinamica: liquidi ad alta velocità ↗  
a bassa velocità ↘ ok



1. liquido incomprimibile:  $\rho = \text{cost} \rightarrow$  si deforma  
ma volume cost

2. liquido non viscoso: trascuro attrito tra elementi  
di fluido vicini



1.+2. liquido  
ideale

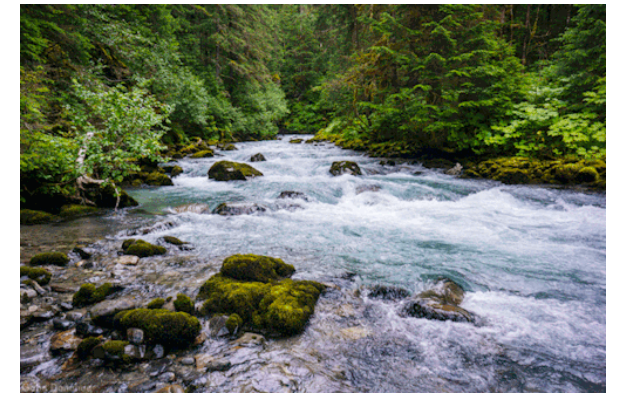
3. corrente stazionaria  $\vec{v}(\vec{r})$  indep. da t

4. corrente irrotazionale  $\rightarrow$  no rotazione

corrente  $\equiv$  flusso



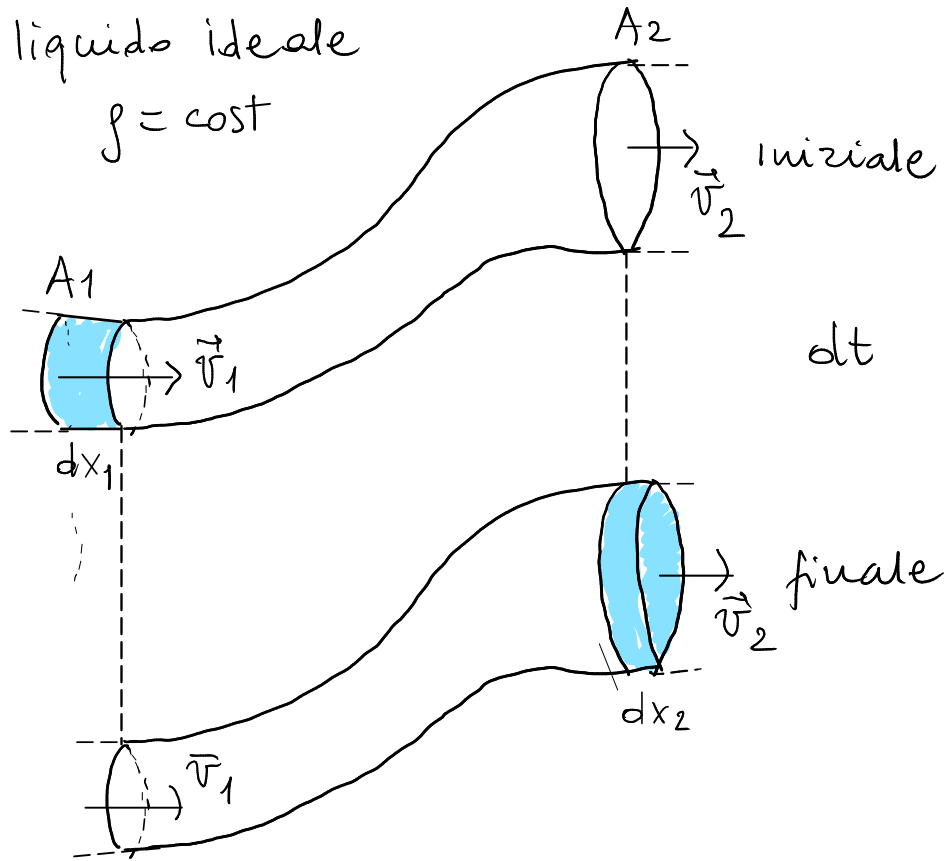
3. + 4.



3.   
4.

# Equazione di continuità per fluidi incompressibili:

liquido ideale  
 $\rho = \text{cost}$



$$\rho A_1 dx_1 = \rho A_2 dx_2$$

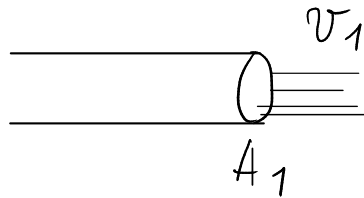
$$\rho A_1 |\vec{v}_1| dt = \rho A_2 |\vec{v}_2| dt$$

$$\Rightarrow A_1 |\vec{v}_1| = A_2 |\vec{v}_2|$$

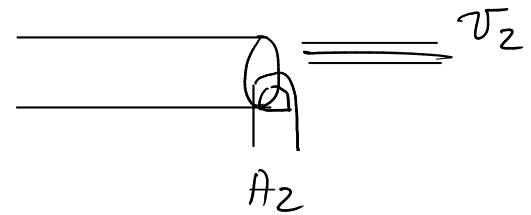
$$\underline{A_1 v_1 = A_2 v_2} \quad \text{eq. continuità}$$

$$[A v] = \frac{L^3}{T} \quad \text{SI: } \frac{m^3}{s}$$

portata  
 o corrente di volume



$$\underline{v_2 = \frac{A_1}{A_2} v_1}$$



$$A_2 = \frac{1}{2} A_1 \Rightarrow v_2 = 2 v_1$$



$$\textcircled{2} \quad W[\vec{g}] = -\Delta E_p$$

$$\Delta E_p = (mg y_2 + E_p^0) - (mg y_1 + E_p^0) = mg(y_2 - y_1)$$

$$\textcircled{3} \quad \Delta E_c = \left( \frac{1}{2} m v_2^2 + E_c^0 \right) - \left( \frac{1}{2} m v_1^2 + E_c^0 \right) = \frac{1}{2} m v_2^2 - \frac{1}{2} m v_1^2$$

$$\Delta E_c + \Delta E_p = W_1 + W_2$$

$$\frac{1}{2} m v_2^2 - \frac{1}{2} m v_1^2 + mg y_2 - mg y_1 = P_1 V - P_2 V \quad / V \quad \frac{m}{V} = \rho$$

$$\frac{1}{2} \rho v_2^2 + \rho g y_2 + P_2 = \frac{1}{2} \rho v_1^2 + \rho g y_1 + P_1 \Rightarrow \frac{1}{2} \rho v^2 + \rho g y + P = \text{cost}$$

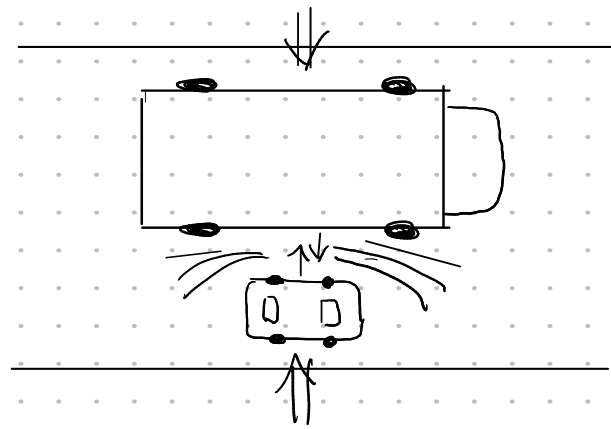
Casi particolari:

$$1) \quad v_1 = v_2 = 0 \Rightarrow P_2 + \rho g y_2 = P_1 + \rho g y_1 \Rightarrow P_2 = P_1 + \rho g \Delta y$$

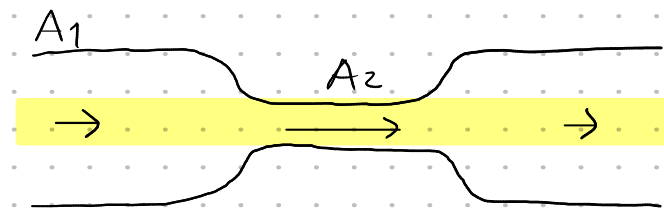
liquido statico

$$P = P_0 + \rho g \Delta y \quad \text{Stevin}$$

$$2) \quad y_1 = y_2 = \text{cost}$$



effetto Venturi

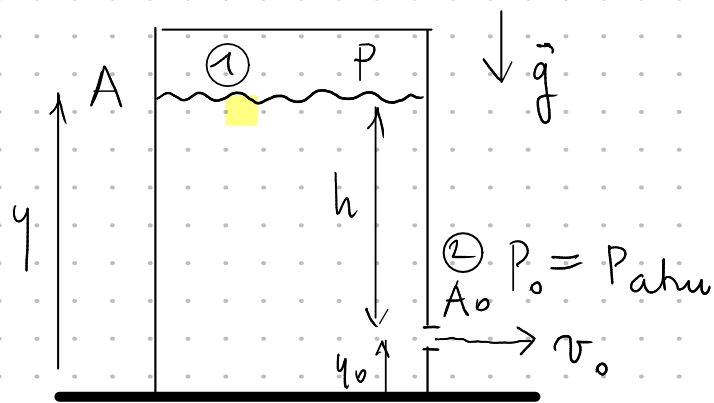


$$\frac{1}{2} \rho v^2 + P = \text{cost}$$

eq. continuità:  $A_1 v_1 = A_2 v_2$

$$v_2 = \frac{A_1}{A_2} v_1$$

Esempio:  $g = \text{cost}$      $h = y - y_0$      $\Rightarrow v_0 = ?$



$\sim$  estatore

Bernoulli:

$$\frac{1}{2} \rho v^2 + \rho g y + P = \frac{1}{2} \rho v_0^2 + \rho g y_0 + P_0$$

①

②

$A \gg A_0 \Rightarrow v \approx 0$

$$\rho g y + P = \frac{1}{2} \rho v_0^2 + \rho g y_0 + P_0$$

$$\frac{1}{2} \rho v_0^2 = (P - P_0) + \rho g (y - y_0) = (P - P_0) + \rho g h$$

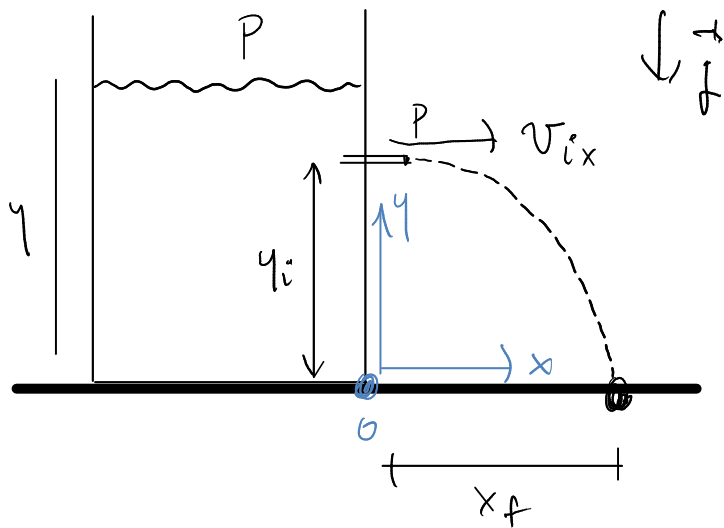
$$v_o^2 = 2 \frac{P-P_o}{\rho} + 2gh \Rightarrow$$

$$v_o = \sqrt{2 \frac{P-P_o}{\rho} + 2gh}$$

-  $P \gg P_o \Rightarrow v_o \approx \sqrt{2 \frac{P-P_o}{\rho}}$

- contutore aperto  $\Rightarrow P = P_o \Rightarrow v_o = \sqrt{2gh} \rightarrow$  caduta libera! legge di Torricelli

Variante: contutore aperto,  $\rho = \text{cost}$   $\Rightarrow y_i$  tale che gittata  $x_f$  è massima?



$$v_{ix} = \sqrt{2gy_i}$$

$$\begin{cases} y = y_i + v_{iy}t - \frac{1}{2}gt^2 = y_i - \frac{1}{2}gt^2 \\ x = x_i + v_{ix}t = \sqrt{2gh} \cdot t = \sqrt{2g(y - y_i)} \end{cases}$$

$$0 = y_i - \frac{1}{2}gt_f^2 \Rightarrow t_f = \sqrt{2gy_i}$$

$$\begin{aligned} x_f &= \sqrt{2g(y - y_i)} \sqrt{2gy_i} = 2g \sqrt{(y - y_i)y_i} \\ &= 2g \sqrt{yy_i - y_i^2} \rightarrow \text{gittata} \end{aligned}$$