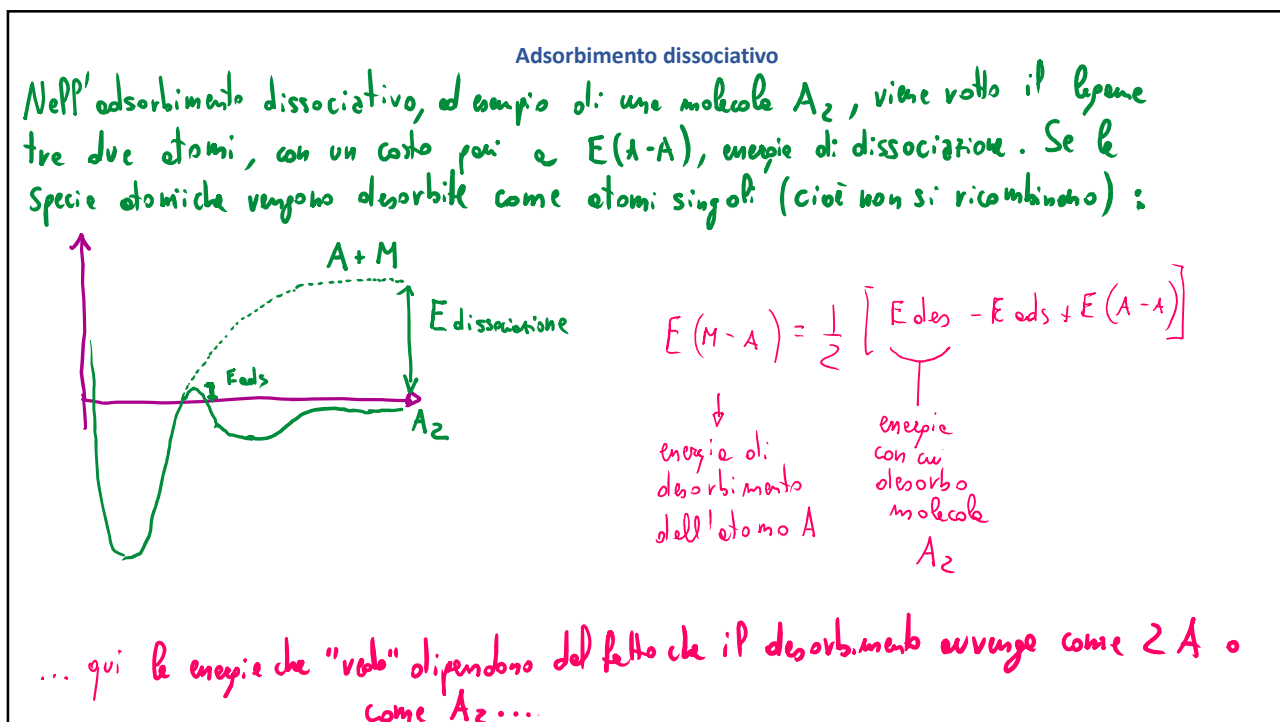
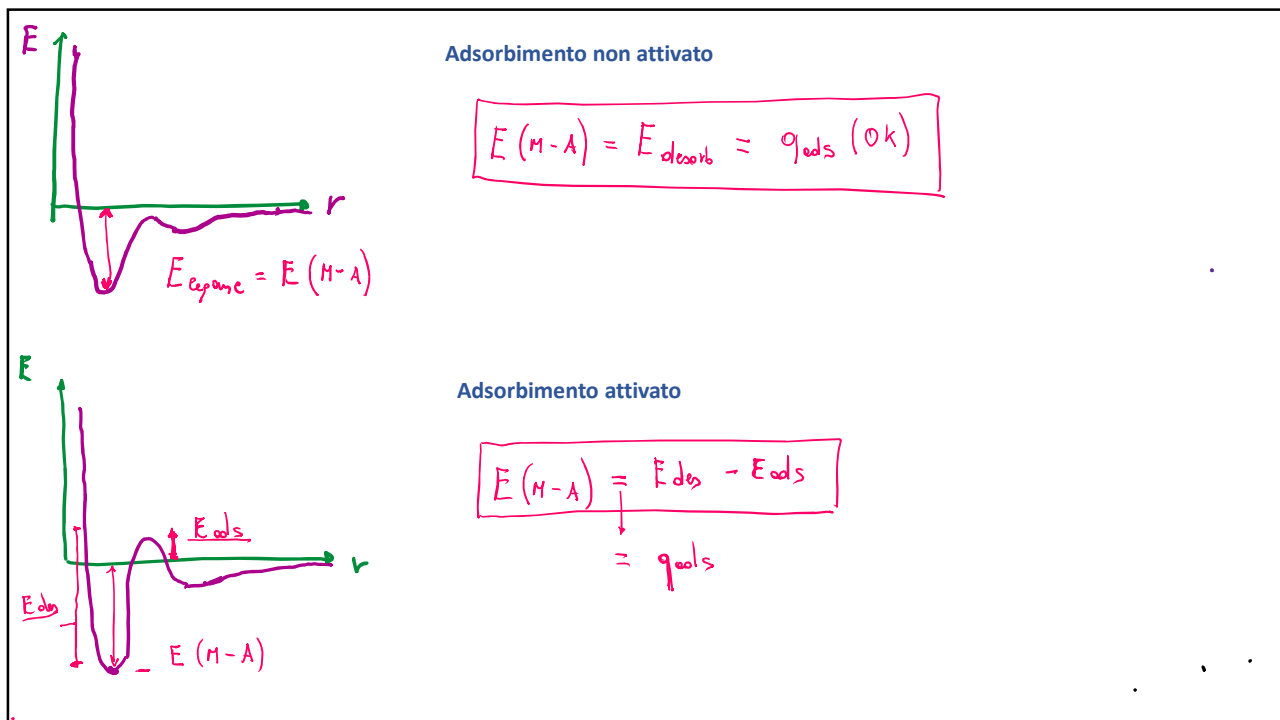




Da un punto di vista termodinamico, essendo l'adsorbimento energeticamente favorito, si ha:

$$\Delta G < 0$$

ma

$$\Delta G = \Delta H - T\Delta S$$

entropia

$S \propto \ln N_c$, N_c numero di configurazioni possibili.

Passando da fase gassosa a fase adsorbibile, N_c diminuisce, sto ordinando il sistema

$$\Rightarrow \Delta S_{ads} < 0$$

$$\Rightarrow \Delta H < 0$$

L'adsorbimento è una reazione
ESOTERMICA

$$H = U + pV$$

gas ideale

$$H_g = U_g + p_g V_g = U_g + RT \quad (n=1, 1 \text{ mole})$$

per l'adsorbato U_a è trascurabile

$$H_a = U_a$$

$$\begin{aligned} (\Delta H)_{ads} &= H_a - H_g = U_a - U_g - \underbrace{RT}_{\sim 2.5 \text{ kJ/mol}} \\ &= -q_{ads} \end{aligned}$$



$q_{ads} \equiv q_{st}$ calore isoterico di adsorbimento

L'adsorbimento di molecole su una superficie può essere visto come una transizione dalle fasi gassose a quelle liquide. In condizioni di equilibrio, avrà ugual numero di molecole che adsorbono - desorbono e la superficie avrà un certo ricoprimento θ costante.

Il calore isosterico (= a ricoprimento costante) è una quantità che in termodinamica è definita dall'EQUAZIONE di CLAUSIUS-CLAPEYRON:

$$q_{st}(\theta) = - R \left(\frac{\partial \ln p}{\partial (1/T)} \right)_{\theta}$$

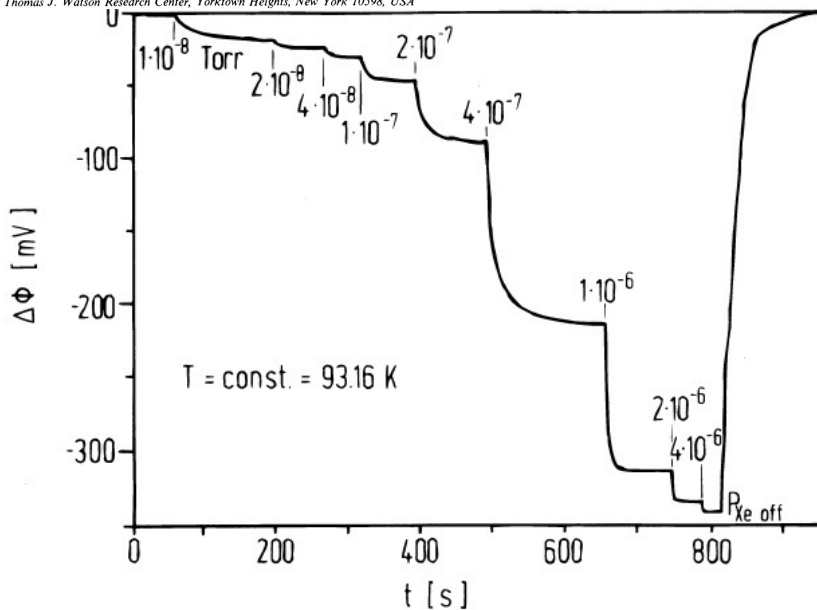
che descrive, in una situazione di equilibrio tra fasi liquide e gassose, la relazione tra p, T .

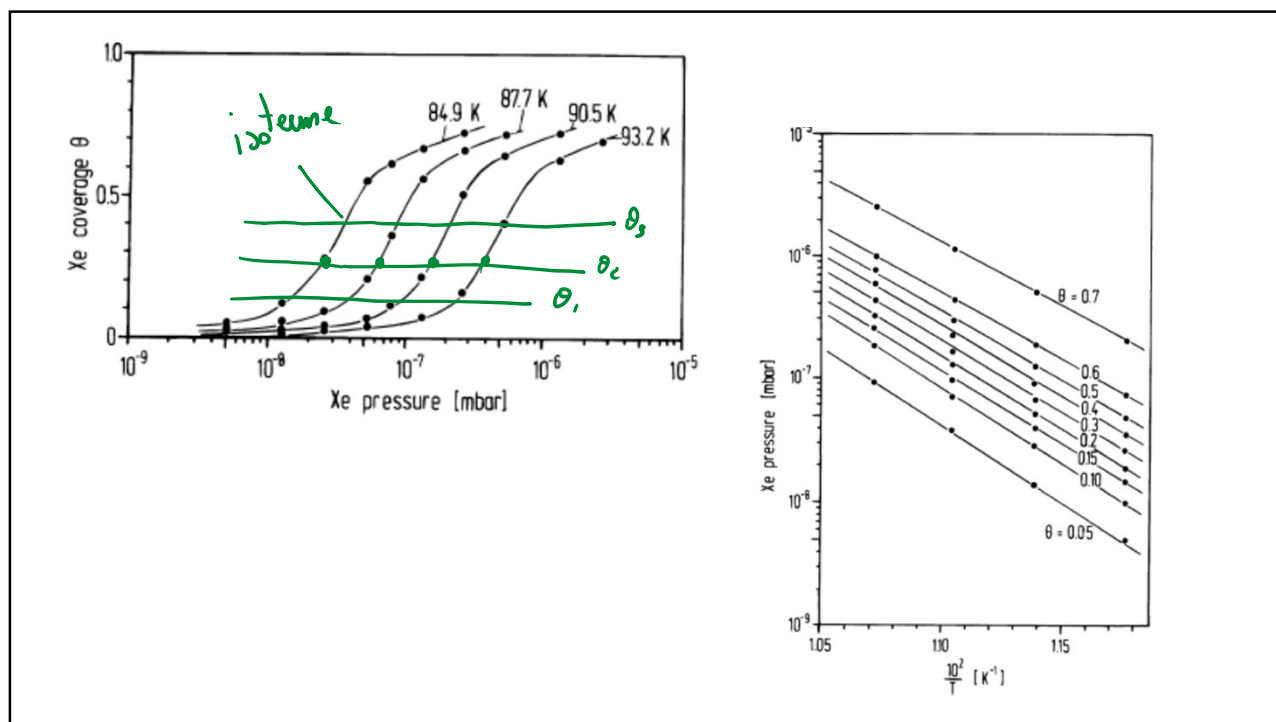
INTERACTION OF INERT GASES WITH A NICKEL (100) SURFACE *

I. Adsorption of xenon

K. CHRISTMANN ** and J.E. DEMUTH

IBM Thomas J. Watson Research Center, Yorktown Heights, New York 10598, USA



Misura di q_{st} Come misuro θ
controllo θ

①

Fotoemissione

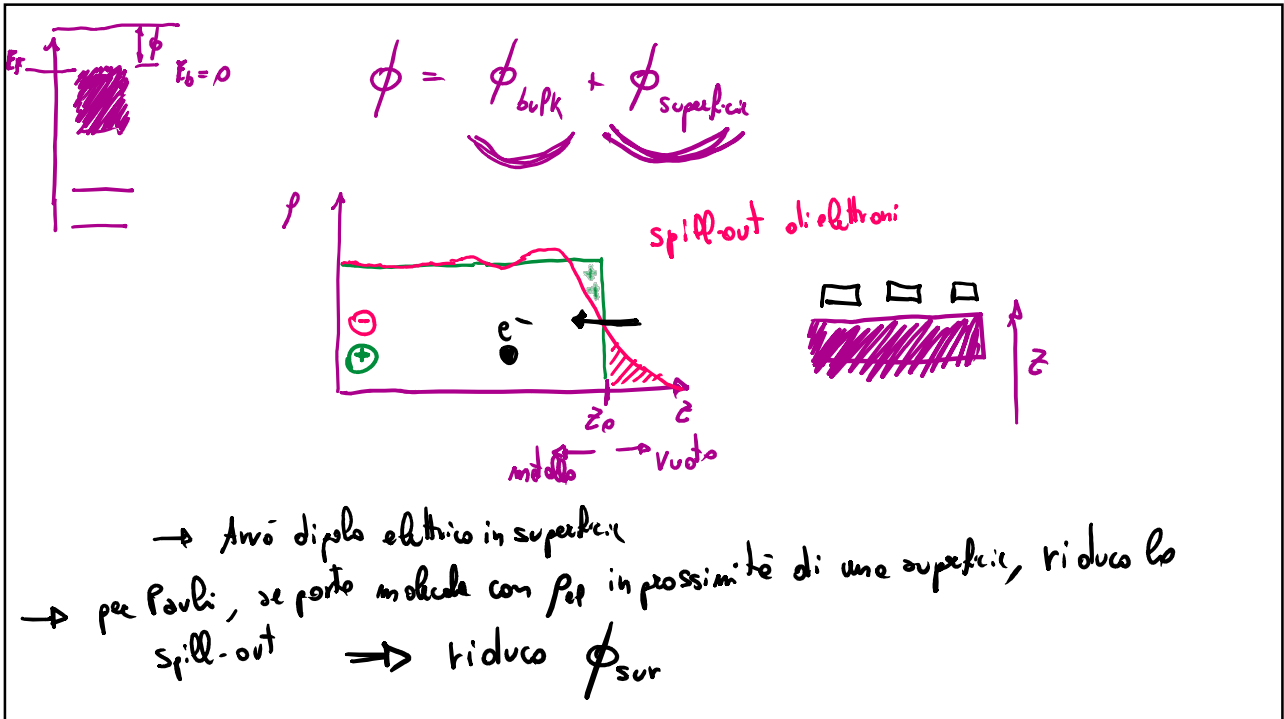
Misura segnale C1s
 $I_{C1s} \propto \theta$ - sorgente fotoni $h\nu$
- analizzatore di e^- 

②

 θ $\propto$ legge $\Delta\phi$ ϕ funzione lavoro

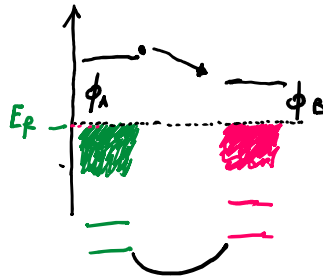
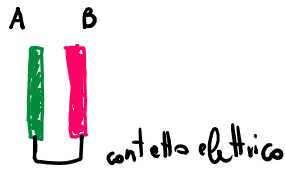
$$h\nu = E_{kin} + E_{bind} + \phi$$

 ϕ cambia $\propto$ dalla molecole si depositano sulla superficie



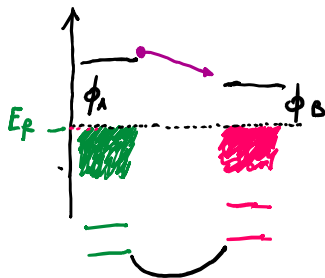
Come si misura la funzione lavoro Φ

Potenziale di contatto (potenziale Volta)



$\phi_A - \phi_B$ è il potenziale Volta

I metodo : fotoemissione



$$h\nu \rightarrow e^-, E_k$$

- $E_{k \max}$: e^- che vivevano a E_F

$$E_{k \max} = h\nu - \phi_A$$

- $E_{k \min}$: $E_k = 0$

per effetto di
urti anelastici



$$E_{k \min} (h\nu - \Delta E_k) = h\nu - (h\nu - \phi_A - 0) = \phi_A$$

II metodo : Kelvin probe

$\Delta\phi$

→ è un condensatore

metto l'elettrodo in vibrazione

ω

$\Rightarrow I \propto \cos(\omega t)$

applico potential opposto

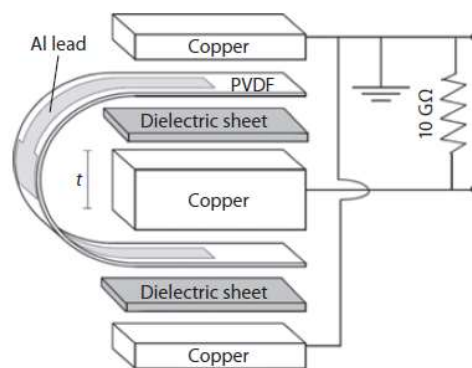
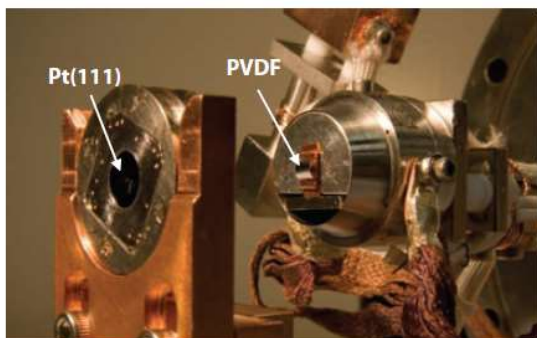
annullo il potential V_{oppt}

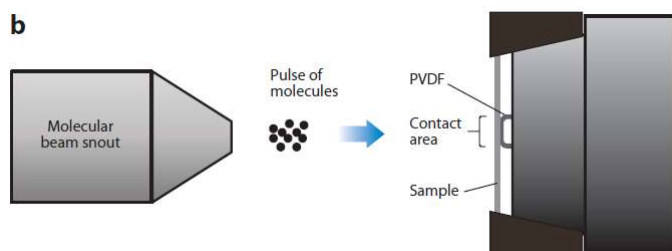
$\Rightarrow I \rightarrow 0$

$\Delta V \propto \Delta\phi_{A-B}$

SCAC Single Crystal Adsorption Calorimetry

PVDF: polimero piezoelettrico $\Delta T \rightarrow \Delta V$

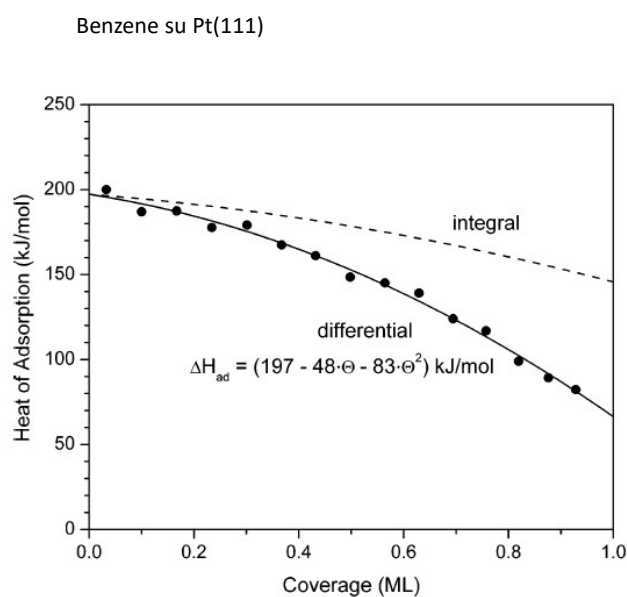




Si usano cristalli
di NaCl

$\text{Pt} \rightarrow \approx 50 \mu\text{m}$
 NaCl

- Calibro la sorgente di molecole in modo da sapere quante molecole arrivano ad ogni pacchetto
- Calibro il mio PVDF, mandando un fascio laser di energia nota per trovare la relazione tra ΔT e ΔV
- Si riesce a determinare: $q_{st} \approx 20-30 \text{ kJ/mol} \pm 2 \text{ kJ/mol}$
risoluzione in T : 0.15 mK



- perché q_{st} dipende da θ ?
- prima saturano siti più reattivi
poi rimangono quelli meno reattivi
- interazione mol-mol diventa importante e $\theta \rightarrow 1$

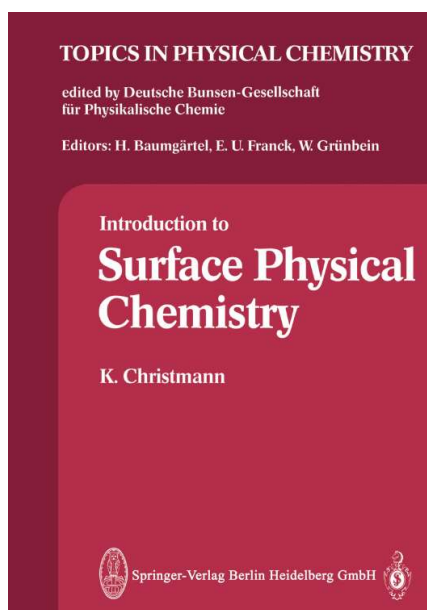
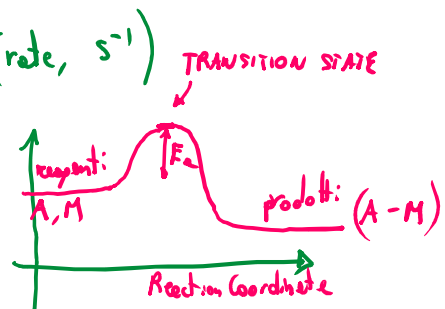
! adsorbimento / desorbimento
 possono essere visti come una reazione
 possono essere descritti dalla equazione (semi empirica) di Arrhenius

$$k = A e^{-\frac{E_a}{RT}}$$

k $\downarrow$ velocità di reazione, prob. di reazione (rate, s^{-1})

A fattore pre-esponenziale

E_a energia di attivazione



Thermal desorption
 Kelvin probe
 Misura di fattore pre-esponenziale

coefficiente di sticking S : rapporto tra il # molecole adsorbite
molecole che collidono

$$0 \leq S \leq 1$$

rate di adsorbimento: mi dice la velocità con cui aumenta σ , ricoprimento di una superficie

$$r_{ad} = S \cdot Z_w = \frac{d\sigma}{dt}$$

$$\sigma = \frac{N_{molecole}}{Area_{sup.}}$$

$$\sigma_0 = \sigma_{MAX}, \frac{\# molecole_{max}}{Area} = \frac{siti di adsorbimento}{Area}$$

$$\frac{\sigma}{\sigma_0} = \theta \quad \text{ricoprimento}$$

$$0 \leq \theta \leq 1$$

Adsorbimento alla Langmuir

$$r_{ad} = Z_w \cdot S(T_s, \theta)$$

$$\theta = \frac{\sigma}{\sigma_0}$$

$$\sigma = N_{molecole}/Area$$

1. $S = 1$ se il sito è libero
 $S = 0$ " " " è già occupato

2. la particella non viaggia sulla superficie su cui atterra

$$S = 1 - \theta$$

ADSORBIMENTO NON DISSOCIATIVO

$$r_{ad} = \frac{P}{\sqrt{2\pi K_B T}} (1 - \theta)$$



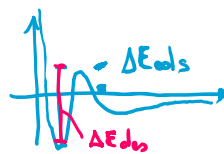
ADSORBIMENTO DISSOCIATIVO

$$S = (1 - \theta)^2$$

Sie per il caso DISSOCIATIVO che per quello NON-DISSOCIATIVO :

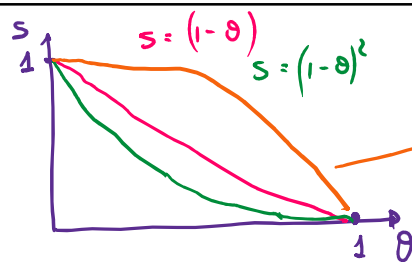
① $S_{\text{iniziale}} < 1$ $S = S_0(1 - \theta)$ caso non diss
 $S = S_0(1 - \theta^2)$ " dissociativo

② ΔE_{ads} barriera di adsorbimento $S \propto e^{-\frac{\Delta E_{\text{ads}}}{RT}}$



↓
ESEMPIO: non dissociativo

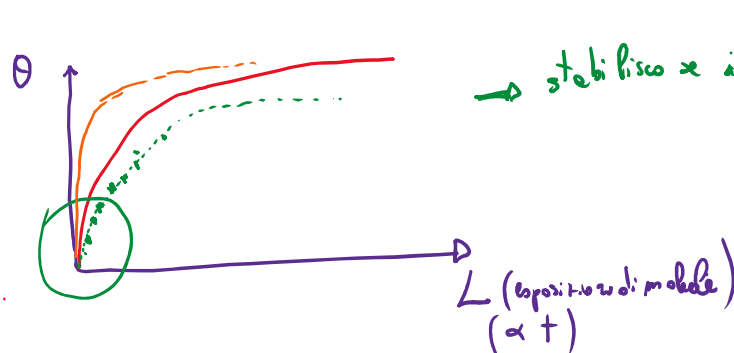
$r_{\text{ad}} = Z_w \cdot S_0(1 - \theta) e^{-\frac{\Delta E_{\text{ad}}}{RT}}$ ← ΔE_{ads} può essere stimato!

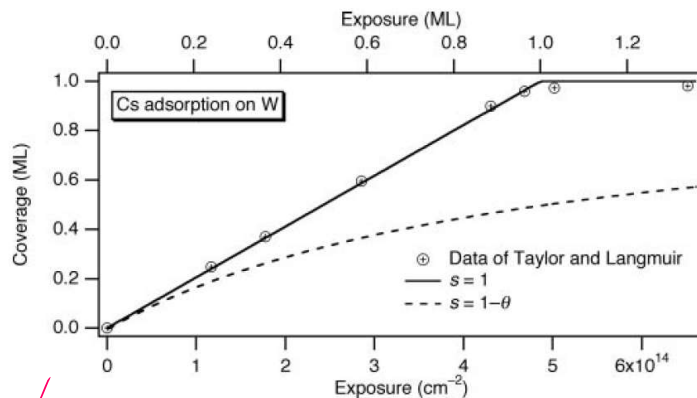


Caso 3:

precursor state
mediato da stato precursor

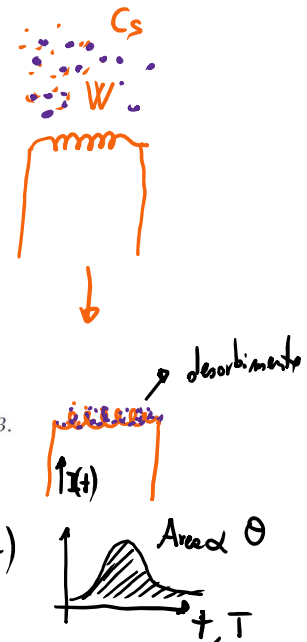
da molecole diffuse
sulla superficie.





Sticking of Cs on W. Replotted from the data of J. B. Taylor, I. Langmuir, Phys. Rev., 44 (1933) 423.

Quindi qui ho un precursor state



IL DESORBIMENTO

Il modo più semplice per descrivere il processo di desorbimento è l'equazione empirica di Frenkel:

Legge di Frenkel (equazione di Frenkel)

$h\nu = kT$ $\nu \approx 10^{13}$
 ν frequenza di vibrazione
 ν sono i tentativi che la molecola fa x scappare

$$\tau_0 = \frac{1}{\nu}$$

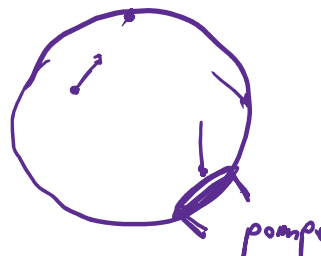
probabilità che la molecola desorba:

$$\tau = \tau_0 e^{\frac{\Delta E_{des}}{kT}}$$

$$\frac{1}{\tau_0} \cdot e^{-\frac{\Delta E_{des}}{kT}} \approx \nu_n$$

Dependence of Stay Time on Binding Energy at Room Temperature

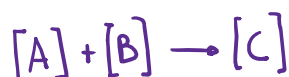
q in kJ mol^{-1}	τ_a
6	1.2×10^{-12} s
15	5×10^{-11} s
40	1.2×10^{-6} s
60	5.5×10^{-3} s
80	15 s
90	15 min
95	2 h
100	8×10^4 s $\sim$ 1 d
120	2×10^8 s $\sim$ 10 years
150	7×10^{13} s $\sim$ 20,000 years

 H_2P DESORBIMENTO

I Prate di desorbimento

$$r_{\text{des}} \equiv -\frac{\partial \sigma}{\partial t} = \underbrace{\nu_n \sigma^n}_{A \text{ (Arrhenius)}} e^{-\frac{\Delta E_{\text{db}}}{RT_s}}$$

A (Arrhenius)

 σ^n n è l'ordine della reazione di desorbimento

$$V = K[A][B] \quad \leftarrow \text{ordine: } 1+1=2$$

$$K = \nu_n e^{-\frac{\Delta E_{\text{db}}}{RT}}$$

Legge di Polanyi-Wigner T_s = Temp. della superficie ν_n = costante pre-exp ΔE_{db} = Energia di desorbimento

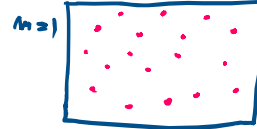
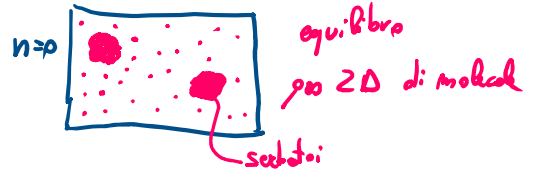
$n=0$

$$r_{d0} = \nu_0 e^{-\frac{E_{d0}}{RT}}$$

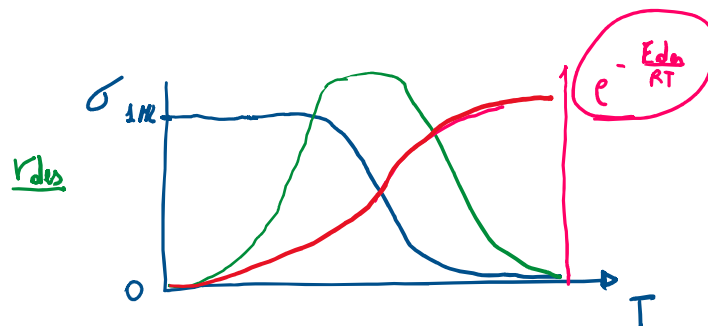
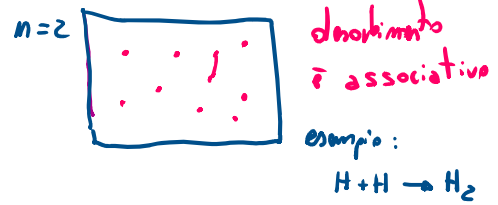
= gas 2D in equilibrio con "seaboi"
= multiple

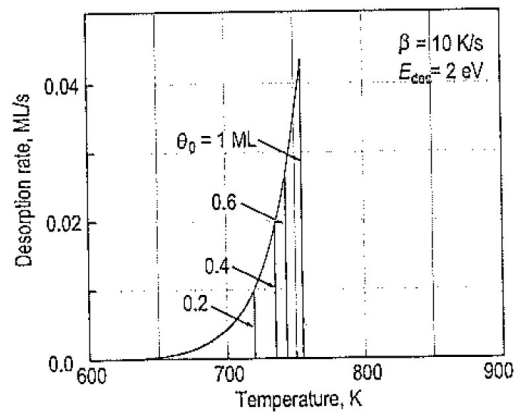
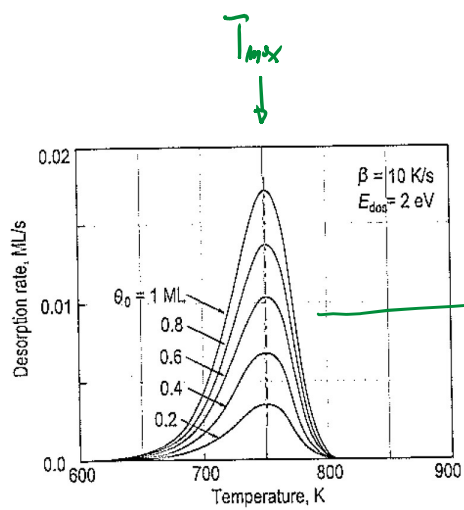
 $n=1$

$$r_{d1} = \nu_1 \sigma \cdot c e^{-\frac{E_{d1}}{RT}}$$

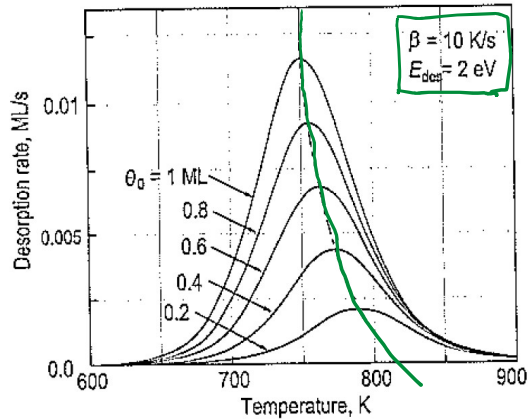
 $n=2$

$$r_{d2} = \nu_2 \sigma^2 e^{-\frac{E_{d2}}{RT}}$$



Zero-order ($n = 0$)First-order ($n = 1$)

picchi asimmetrici



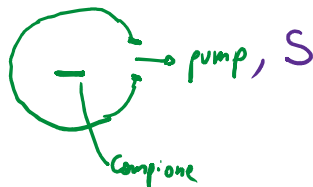
Second-order ($n = 2$)

~ picchi simmetrici

Cambia Tempr d'uscita di $\theta_{iniziale}$

$r_{des} \leftrightarrow P$

Area, A



desorbimento campione

$$\frac{dN(t)}{dt} = -A \frac{d\sigma(t)}{dt} - \underbrace{\left(\frac{dN}{dt} \right)_{\text{pump}}}_{\approx 0} - \cancel{\left(\frac{dN}{dt} \right)_{\text{ads camera}}}$$

velocità di pompaggio

$$S = - \frac{dV}{dt} \Big|_P \Rightarrow S = - \frac{d}{dt} \left(\frac{nRT}{P} \right) = - \frac{RT}{PN_a} \frac{dN}{dt}$$

$$\boxed{\frac{dN}{dt} = -S \frac{P N_a}{RT} = -S \frac{nRT N_a}{RT V} = - \frac{SN}{V}}$$

$$\frac{dN(t)}{dt} = -A \frac{d\sigma(t)}{dt} - S \frac{N(t)}{V}$$

$$\boxed{\frac{dP}{dt} = -\frac{ART}{N_A V} \frac{d\sigma(t)}{dt} - \frac{SP}{V}}$$

$$PV = nRT$$

$$\stackrel{!}{=} \frac{N}{N_A} RT \quad N = PV \frac{N_A}{RT}$$

$$\tau = \frac{V}{S} \quad \text{tempo caratteristico di pompaggio}$$

$$\frac{dP}{dt} = -\frac{ART_m}{N_A V} \frac{d\sigma}{dt} - \frac{P}{\tau}$$

$$\int_0^\infty dt$$

$$P(\infty) - P(0) = 0 = -\frac{ART_m}{N_A V} (\underbrace{\sigma(\infty) - \sigma(0)}_{=0}) - \frac{1}{\tau} \int_0^\infty P(t) dt$$



$$\sigma_{\text{finale}} = \frac{N_A V}{ART_m \tau} \int_0^\infty P(t) dt$$

$$\underbrace{V \frac{dP(t)}{dt}}_{\textcircled{1}} = -\frac{ART}{N_A} \frac{d\sigma}{dt} \stackrel{= r_{\text{des}}}{=} - \underbrace{P(t) \cdot S}_{\textcircled{2}}$$

$S \gg \textcircled{1} \rightarrow$ il primo termine $\textcircled{1}$ è trascurabile rispetto a $\textcircled{2}$

$\Rightarrow$

$$\boxed{r_{\text{des}} \propto P(t)}$$

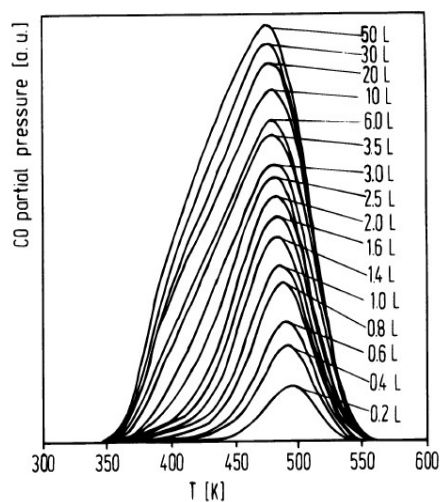


Fig. 4.54. Example for first-order thermal-desorption spectra: CO desorption from a Pd(100) surface. The heating rate β was 14 K/s; CO adsorption was performed at 350 K. The desorption maximum appears, for small coverages, around 490 K and shifts only by ~ 15 K to lower temperatures as coverage increases, indicating first-order kinetic behavior and (almost) constant activation energy for desorption. After Behm et al. [232].

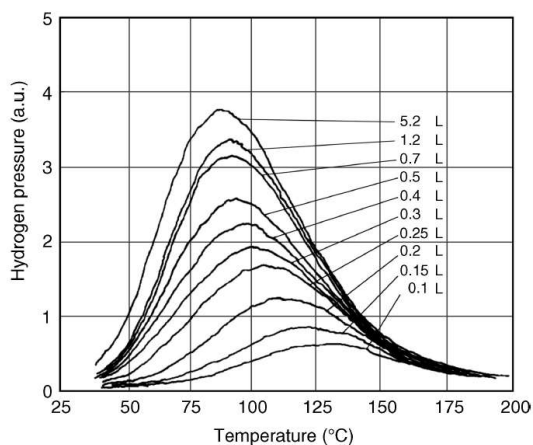
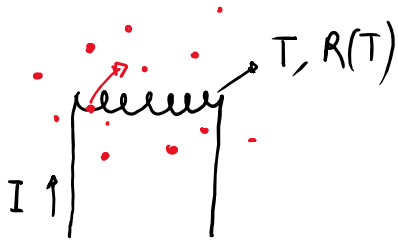


FIGURE 1.5. A series of (second-order) thermal desorption spectra for recombinative desorption of H_2 from an Ni(100) surface. Parameter is the initial exposure in Langmuir [24].

Pirani



l'adsorbimento delle molecole
raffredda il filamento

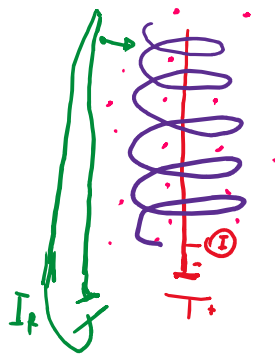
→ deve avere molte molecole/s che interagiscono

→ $\sim 5 \cdot 10^{-9} \text{ mbar} < P < 1000 \text{ mbar}$

Bayard-Alpert



filamento
-30V



collettore

Spirale : potenziale $\oplus$
($\sim 200 \text{ V}$)

e^- → dal filamento vanno
verso la spirale
↓
ionizzano molecole

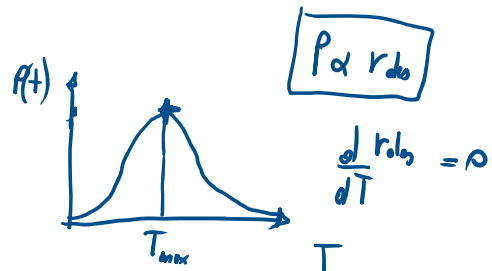
$10^{-10} \text{ mbar} < P < \underline{\underline{10^{-9} \text{ mbar}}}$

Temperature programmed Desorption (TPD)

$$T_s = T_0 + \beta t \rightarrow dT = \beta dt$$

$$r_{des} = -\frac{d\sigma(t)}{dt} = \nu_n \sigma^n e^{-\frac{\Delta E_d}{RT}}$$

$$\frac{d\sigma(t)}{dT} = -\frac{1}{\beta} \nu_n \sigma^n e^{-\frac{\Delta E_d}{RT}}$$



$$\frac{d\sigma(t)}{dT} = -\frac{1}{\beta} \nu_n \sigma^n e^{-\frac{\Delta E_d}{RT}}$$

$$r_{des} = -\frac{d\sigma}{dt} = -\beta \frac{d\sigma}{dT}$$

$$0 = \frac{d r_{des}}{dT} \Big|_{T_{max}} \propto \frac{d}{dT} \left(\nu_n \sigma^n e^{-\frac{\Delta E_d}{RT}} \right) \overset{\nu_n \text{ const. w.r.t. } T}{=} \nu_n \left(\left(\frac{d\sigma^n}{dT} \right) e^{-\frac{\Delta E_d}{RT}} + \sigma^n \frac{\Delta E_d}{RT^2} e^{-\frac{\Delta E_d}{RT}} \right)$$

$$0 = \frac{d}{dT} \sigma^n + \sigma^n \frac{\Delta E_d}{RT^2}$$

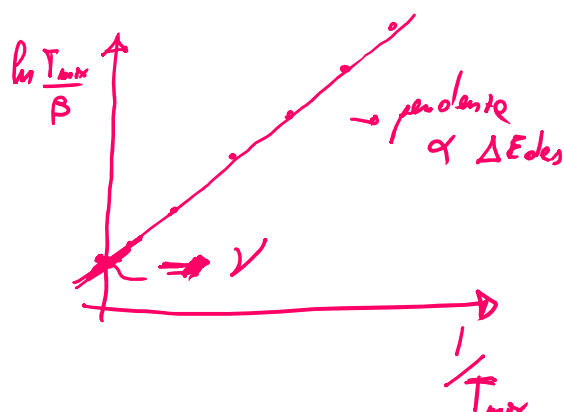
$$= n \sigma^{n-1} \frac{d\sigma}{dT} + \sigma^n \frac{\Delta E_d}{RT^2} = -\frac{n}{\beta} \nu_n \sigma^{n-1} e^{-\frac{\Delta E_d}{RT}} + \cancel{\sigma^n} \frac{\Delta E_d}{RT^2} = 0$$

$$\frac{\Delta E_{des}}{RT_{max}^2} = \frac{1}{\beta} \nu_n \cdot n \cdot \delta^{n-1} e^{-\frac{\Delta E_{des}}{RT}}$$

Case n=1

$$\frac{\Delta E_{des}}{RT_{max}^2} = \frac{1}{\beta} \nu_1 e^{-\frac{\Delta E_{des}}{RT_{max}}}$$

$$\ln \frac{T_{max}^2}{\beta} = \frac{\Delta E_{des}}{RT_{max}} + \ln \frac{\Delta E_{des}}{\nu_1 R}$$



Adsorption of CO on Pd(100)

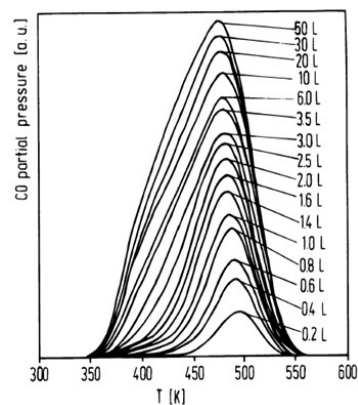
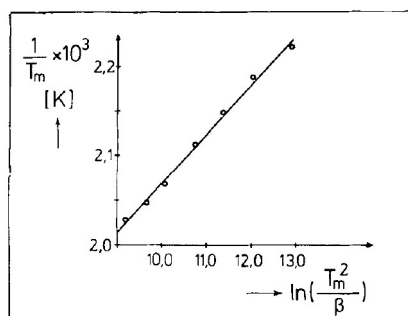
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(Received 4 February 1980; accepted 19 May 1980)

J. Chem. Phys., Vol. 73, No. 6, 15 September 1980



For $\theta = 0.13 \text{ ML}$:

$$\nu = 2 \cdot 10^{16} \text{ s}^{-1}$$

$$E_d = 36.8 \text{ Kcal/mole}$$

Desorption Kinetics of Benzene and Cyclohexane from a Graphene Surface

DOI: [10.1021/acs.jpcc.7b05102](https://doi.org/10.1021/acs.jpcc.7b05102)

R. Scott Smith* and Bruce D. Kay*

J. Phys. Chem. B 2018, 122, 587–594